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# Role of Calorimetry in the study of Adsorption and Adsorbents

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# Role of Calorimetry in the study of Adsorption and Adsorbents

A/ Introduction to calorimetry and calorimeters

B/ Experimental procedures of adsorption and immersion, derivation of thermodynamic quantities

C/ Applications of gas adsorption calorimetry

D/ Applications of immersion calorimetry

# A/ Introduction to calorimetry and calorimeters

1/ Definition, objective, strength and difficulties of calorimetry

2/ General presentation and classification of calorimeters

3/ Selection of those suited for gas adsorption calorimetry and immersion calorimetry

# 1/ Definition, objective, strength and difficulties of calorimetry

- ⌘ « Calorimeter » : term coined in 1789 by Lavoisier to designate an equipment able to measure heat
- ⌘ The objective is to **better understand a phenomenon** (like adsorption) after the measurement of the **heat exchanged**
- ⌘ This requires assessing the changes of a **state function** ( $U, H, S$ )
- ⌘ One should then fully control the **initial state** (synthesis, sampling, outgassing,  $P, T...$ ) and the **final state** (amount adsorbed,  $P, T...$ )
- ⌘ One should also fully control the calorimetric experiment proper, to be able to derive a state function (isothermicity, reversibility)

# A/ Introduction to calorimetry and calorimeters

1/ Definition, objective, strength and difficulties of calorimetry

2/ General presentation and classification of calorimeters

3/ Selection of those suited for gas adsorption calorimetry and immersion calorimetry

## 2/ General presentation and classification of calorimeters

### a) A good clarification is requested

- ⌘ «More than 100 different types of calorimeters invented, in 200 years, to « catch » the heat
- ⌘ More than 10 different classifications were proposed
- ⌘ This makes that the student - but usually also the teacher - has much difficulties to have a clear view about calorimetry

**1st example of confusion:  
so many calorimeters and so many names !**

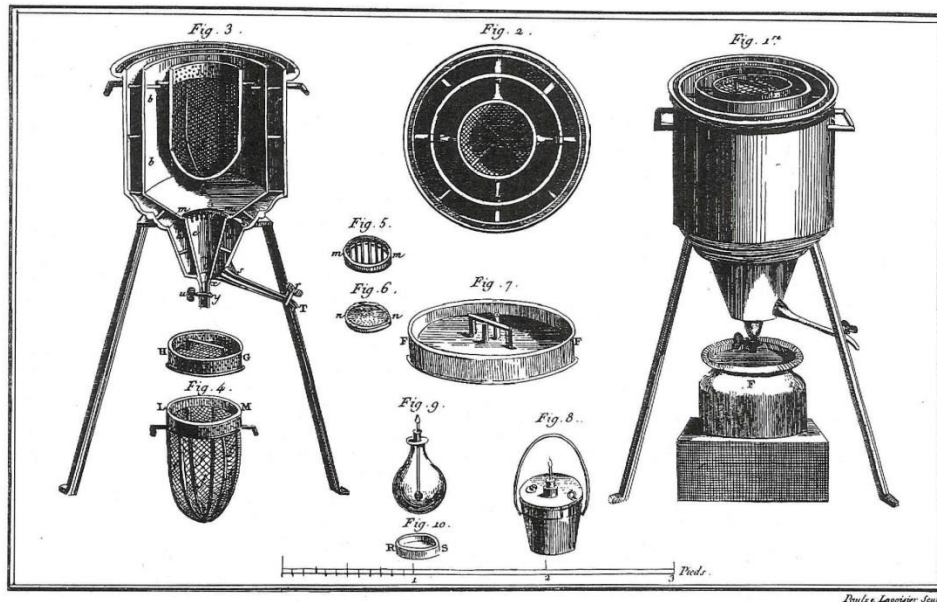
« reaction », « isothermal », « ice », « drop »,  
« temperature jump », « solution », « liquid  
flow », « heat flow », « stop flow », « adiabatic »,  
« ordinary », « AC », « laser flash », « battery »  
« flame », « combustion », « cone »,  
« conduction », « deformation », « thermopile »,  
« bomb », « pneumatic », « mixing »,  
« biocalorimeter », « photocalorimeter », « surface  
calorimeter » etc...



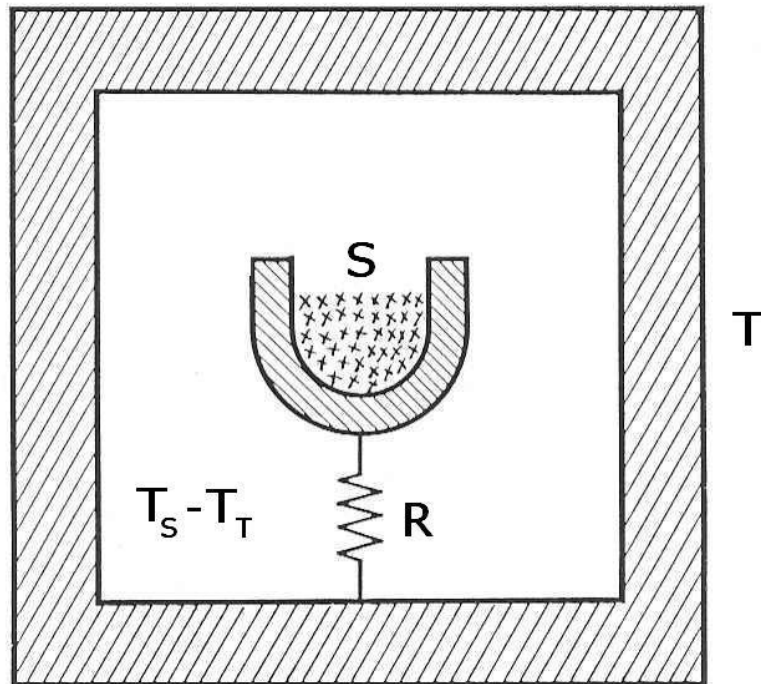
*2<sup>nd</sup> example of confusion: even a single calorimeter is described in many different ways, sometimes inconsistent with each other*

*For instance, Laplace and Lavoisier's ice calorimeter is classified as:*

- Phase change*
- Isothermal*
- Conduction*
- Compensation*
- Adiabatic*



b) A simple classification is requested, which starts with the schematic representation of a calorimeter



- ⌘ S : system made up of the sample and its container or vessel (with which it is in good thermal contact)
- ⌘ T : surrounding thermostat (characterized by its temperature  $T_T$ )
- ⌘ R : thermal resistance through which the heat exchanges between S and T occur
- ⌘  $T_S - T_T$  : temperature difference between S and T

# Extreme modes of operation of calorimeters after the heat exchange

⌘ **Adiabatic mode** ( $\alpha\delta\iota\alpha\beta\alpha\tau\omicron\zeta$ , *adiabatos*, «which cannot be crossed»)

No heat exchange between the system and the thermostat

⌘ **Diathermal mode** ( $\delta\iota\alpha\alpha$ , *dia*, « through », and  $\theta\epsilon\rho\mu\omicron\sigma$ , *thermos*, « hot » )

The whole energy involved by the system transformation is exchanged with the thermostat

# Classification of real calorimeters: 2 groups, 4 categories

Adiabatic calorimeters

1/« active »

2/« passive »

Diathermal calorimeters

1/ « active »

2/ « passive »

# Classification of real calorimeters: 2 groups and 4 categories

## A/ **Adiabatic** calorimeters

- 1/ « active » : heat exchange minimized by servo-controlling the thermostat T after the sample T (« true » adiabatic)
- 2/ « passive » : heat exchange simply minimized by thermal insulation between sample and thermostat (« quasi » adiabatic or isoperibolic: Berthelot, Thomsen, « water calorimeter »)

## B/ **Diathermal** calorimeters

- 3/ « passive » : heat exchange favoured by simple thermal conduction (ex ; Tian-Calvet heat flowmeters, phase-change)
- 4/ « active » : heat exchange replaced by an *in-situ* power compensation which mimics a good thermal conduction (ex: heat flowmeter with Peltier compensation)

Applying this classification with special attention to the calorimeters used for adsorption or immersion studies

# 1/ « Active » adiabatic calorimeters

(« true » adiabatic) (continued)



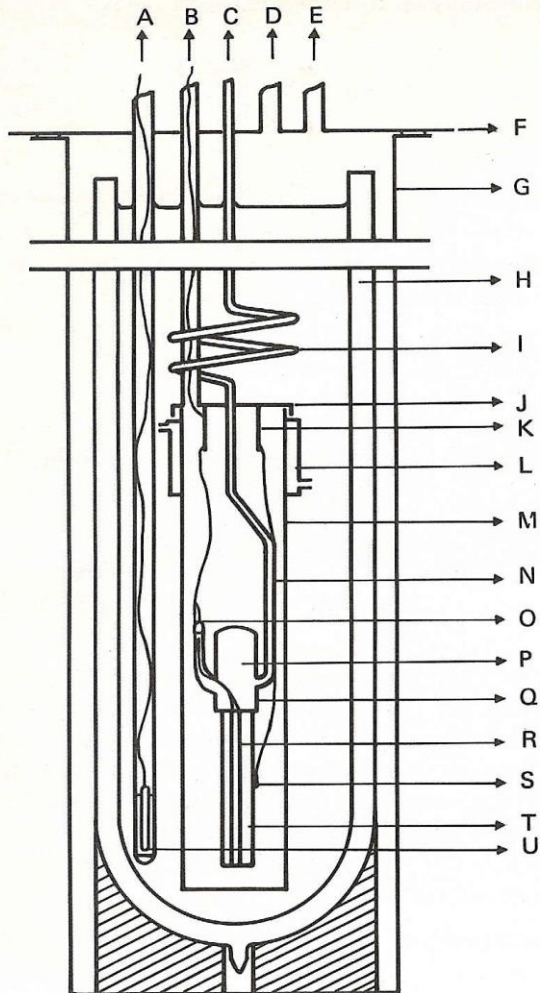
- z Heat exchange minimized by servo-controlling the thermostat temperature after the sample temperature

## Typical examples

Low temperature calorimeters, with multiple shields in vacuum (Westrum, Suga, Grönvold, Gmelin...)



G.L.Kington and P.S.Smith, in 1964, set up a low-temperature, active adiabatic adsorption calorimeter, with vacuum insulation and automatic cancellation of  $\Delta T$ .



## Issues:

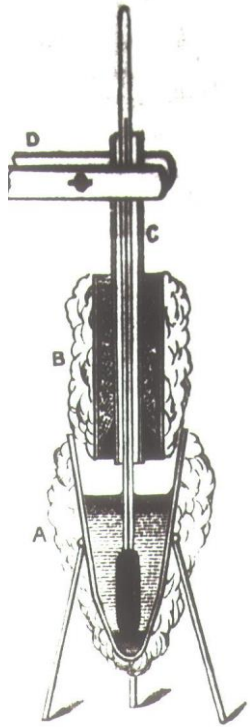
- Adsorptive introduced through thin capillary « C » (needed to lower heat leaks), which impedes correct outgassing and controlled starting state
- Non isothermal, by principle
- Heavy to handle: sample in center of several air-tight containers



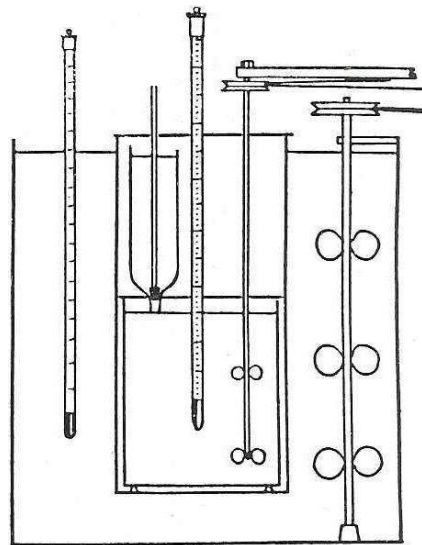
## 2/ « Passive » adiabatic calorimeters

(« quasi-adiabatic », « isoperibol »)

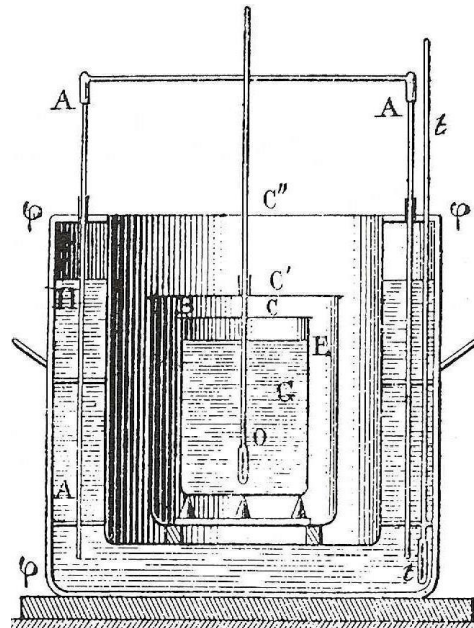
- ⌘ Heat exchange is minimized by thermal insulation
- ⌘  $dQ_{\text{exp}} = dQ_{\text{stored}} + dQ_{\text{exchanged}}$  (corrective term for heat losses)
- ⌘ No mutual dependence between  $T_S$  and  $T_T$  (no coupling)



Pouillet 1822



Thomsen, 1869



Berthelot, 1870

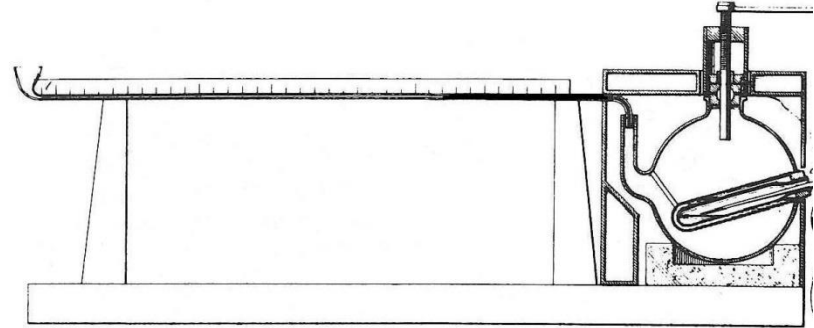
Typical examples:

« Water »  
calorimeters:

Pouillet (immersion)  
Zettlemoyer (immersion)  
Thomsen (reaction)  
Berthelot (bomb)

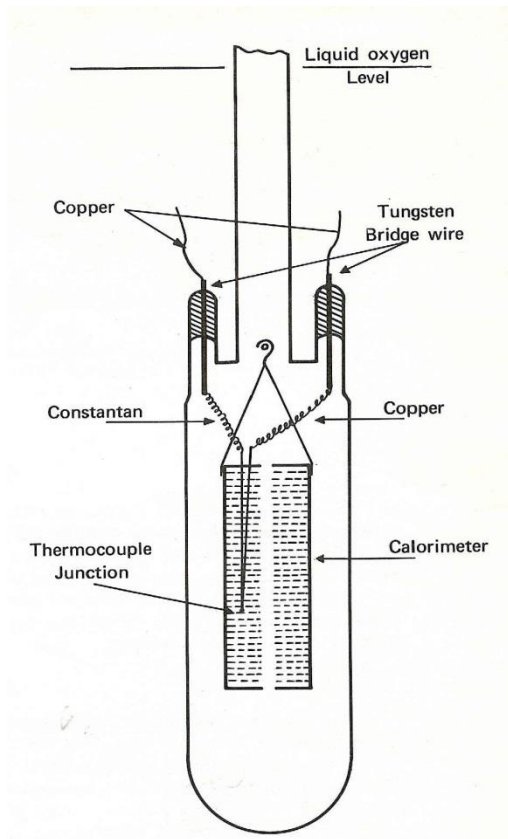
⌘ *Pierre-Antoine Favre made use of 2 quasi-adiabatic calorimeters: one with a mercury thermometer whose bulb (with 10kg mercury!) was the calorimeter proper, the other a standard « water calorimeter » insulated with swan feathers.*

Mercury **dilatation** calorimeter  
(Favre, 1846)



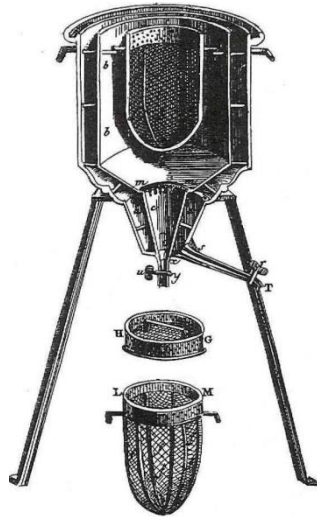
- He was the first to measure **heats of adsorption of gases** ( $\text{SO}_2$ ,  $\text{NH}_3$ ,  $\text{HCl}$ ,  $\text{NO}$ ,  $\text{CO}_2$ ) on solids (charcoals) between 1854 and 1871 (« wetting of solids by gases »)
- 1st Professor of Chemistry of the Faculty of Sciences of Marseilles

➤ **Ralph Beebe** devised, around 1950, a quasi-adiabatic, low-temperature, adsorption calorimeter immersed into liquid oxygen or nitrogen



- Insulation is provided by gaseous adsorptive surrounding the sample cell
- Issue: insulation varies when adsorptive pressure increases and experiment is non-isothermal

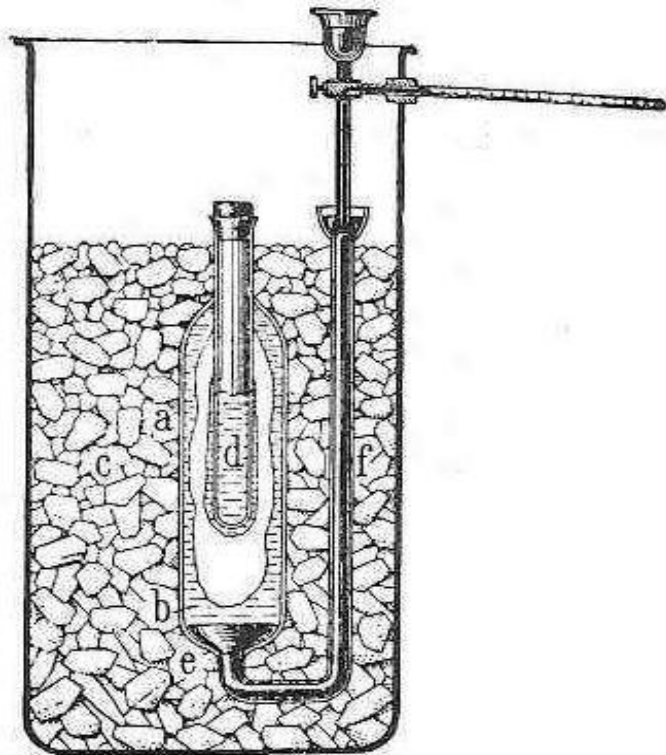
# 3/ « Passive » diathermal calorimeters (« thermal conduction ») with phase change



Lavoisier 1783

- ⌘ Good heat exchange thanks to thermal conduction
- ⌘ Sample temperature passively follows that of the thermostat
- ⌘  $dQ_{\text{stored}} \ll dQ_{\text{exchanged}}$  so that  $dQ_{\text{exp}} \approx dQ_{\text{exchanged}}$
- ⌘  $dQ_{\text{exchanged}}$  measured by help of a **phase change**
- ⌘ Typical: Lavoisier ice calorimeter, 1783)

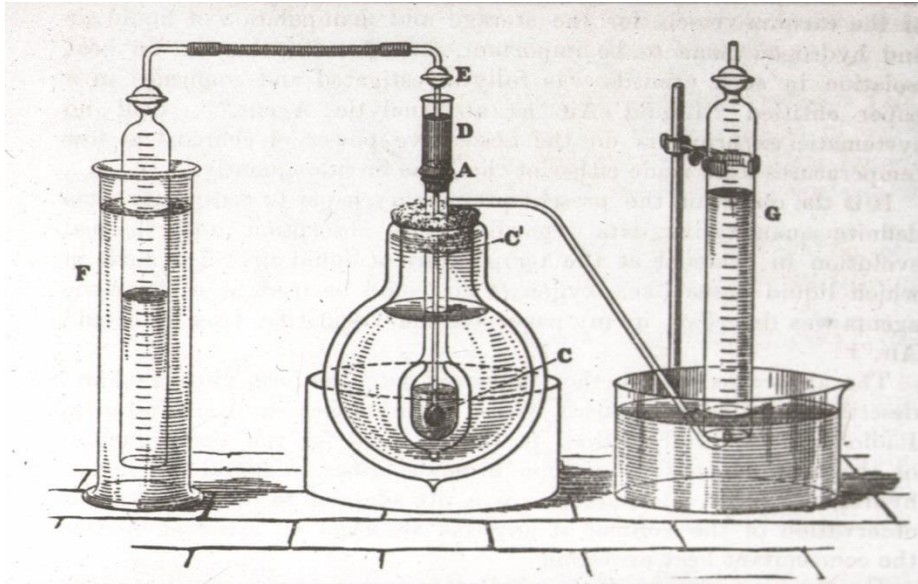
- **Robert Wilhelm Bunsen** devised an **ice calorimeter** later used (until 1975) for adsorption studies because it was **isothermal and sensitive**.
- *Converted measurement of heat into measurement of length (contraction on ice melting followed by mercury in capillary)*



- Improved by use of **diphenyl-ether** (melts at  $27^{\circ}\text{C}$  and expands on melting, hence more regular displacement of mercury index)
- Issue: **limited autonomy** and most « **temperamental** » (after J.Gregg),



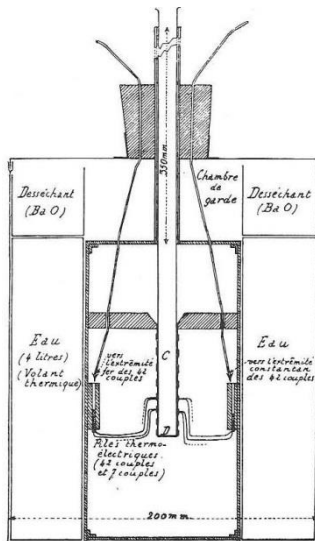
➤ **James Dewar** devised, in 1905, a smart, adsorption calorimeter in liquid air : left buret measures consumption of adsorptive, right buret measures production of air by vapourization (type: passive diathermal with phase-change)



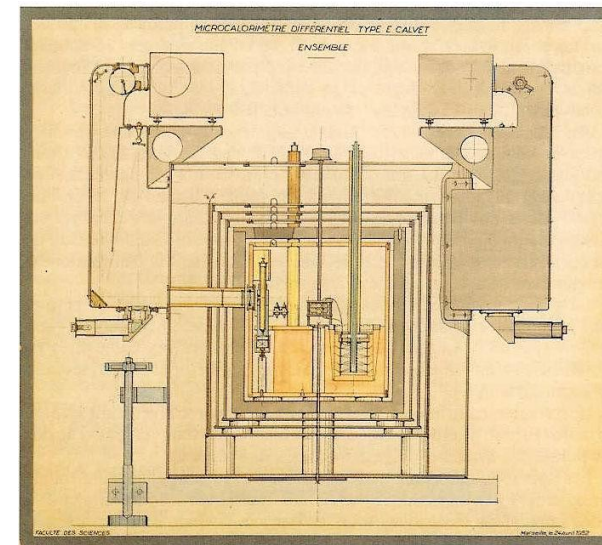
- Later improved by replacing liquid air by liquid nitrogen
- Issue: **limited autonomy** and poor stability, since most sensitive to fluctuations of atmospheric pressure

# 4/ « Passive » diathermal calorimeters (« thermal conduction ») with heat flowmeter

- ⌘ Good heat exchange thanks to thermal conduction
- ⌘ Sample temperature passively follows that of the thermostat
- ⌘  $dQ$  stored  $\ll dQ$  exchanged so that  $dQ_{exp} \approx dQ_{exchanged}$
- ⌘  $dQ$  exchanged measured by **heat flowmeter** (Tian-Calvet, 1923-1948, Wadsö, 1968,)



Tian 1923



Tian-Calvet 1950

Albert Tian (1880 - 1972)



- ⌘ Professor of Chemistry at the Faculty of Sciences of Marseille (1921-1950)
- ⌘ Invented the **heat-flux microcalorimeter**: isothermal, with a thermopile of 42 + 7 thermocouples and with Joule or Peltier power compensation
- ⌘ Invented the **multi-shielded thermostat** (stable within  $10^{-6}$  K) used by A.F.H.Ward, under his guidance, in 1930 (adsorption calorimetry of  $H_2$  on copper)
- ⌘ Launched a school of microcalorimetry...

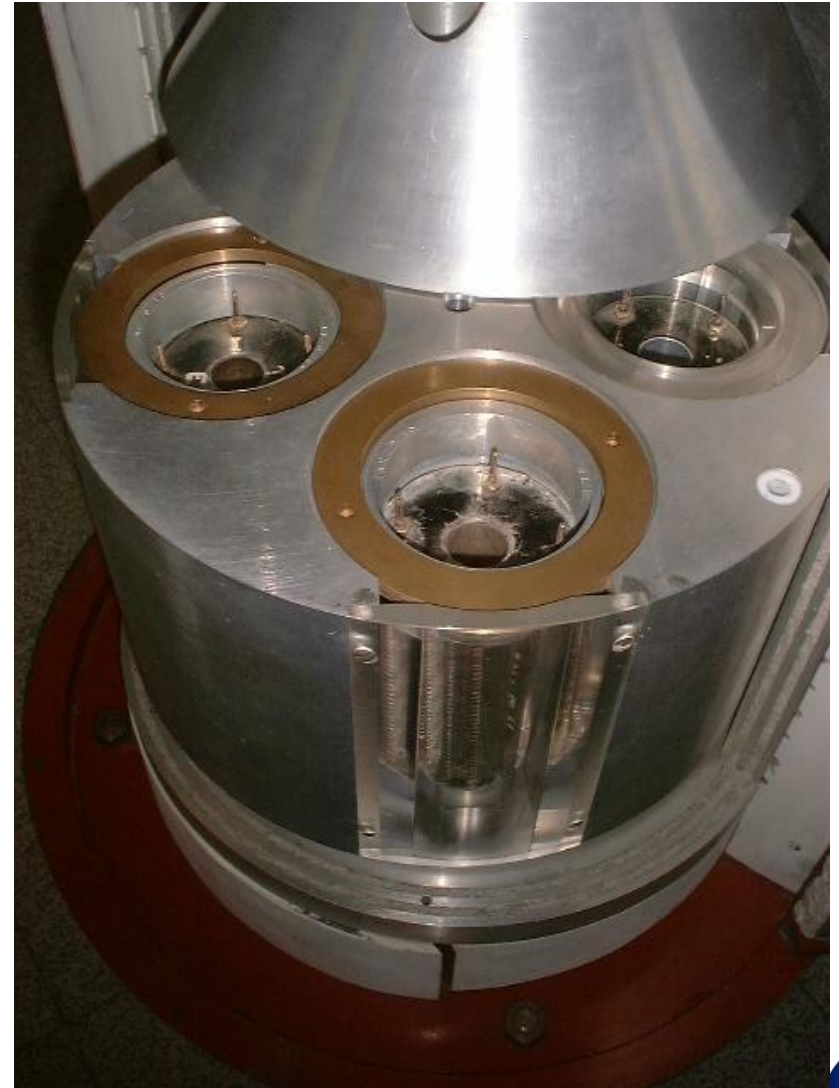


Edouard Calvet  
(Marseille, 1895-1966)

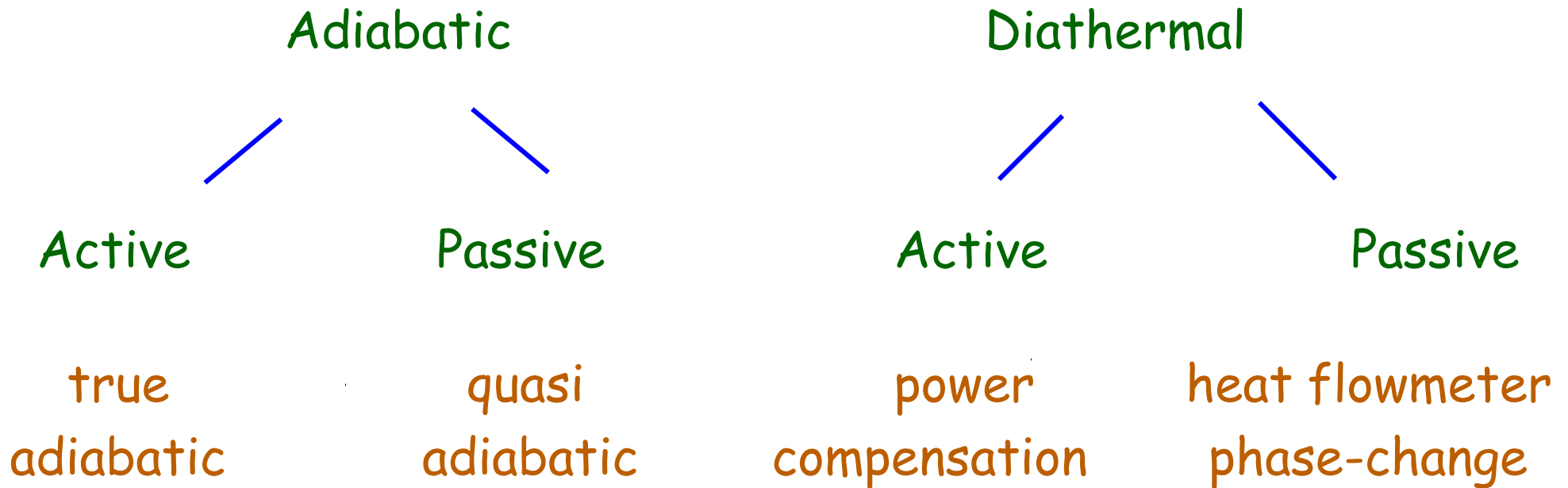


- ⌘ A. Tian 's student, and then successor
- ⌘ Introduced, in 1947, the differential mounting
- ⌘ Made the Tian-Calvet microcalorimeter an extremely versatile piece of equipment
- ⌘ Had a special Institute built by the CNRS, in 1959, for the development of microcalorimetry

# The Tian-Calvet microcalorimeter



Finally, for a simple introduction to calorimetry,  
the following scheme may be enough:



# A/ Introduction to calorimetry and calorimeters

1/ Definition, objective, strength and difficulties of calorimetry

2/ General presentation and classification of calorimeters

3/ Selection of those suited for gas adsorption calorimetry and immersion calorimetry

### 3/ Selection of the calorimeters most suited for: **a) adsorption calorimetry**

- ⌘ Active adiabatic calorimeters :
  - ⌘ OK to measure heat capacity of adsorption system vs  $T$ , to study phase changes
  - ⌘ But for *one composition* of the system (closed system)
  - ⌘ Problems of outgassing
- ⌘ Passive adiabatic calorimeters (Favre, Beebe)
  - ⌘ Non isothermal: experiment ends at higher  $T$ , desorption
- ⌘ Passive diathermal with phase change (Bunsen, Dewar)
  - ⌘ Limited autonomy and choice of  $T$ , delicate to operate
- ⌘ Passive diathermal with heat flowmeter
  - ⌘ Open systems, large choice of  $T$ , high stability and sensitivity (when differential)

### 3/ Selection of the calorimeters most suited for: **b) immersion calorimetry**

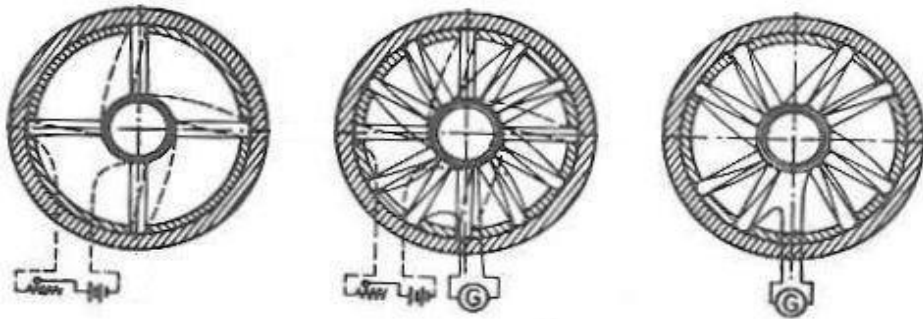
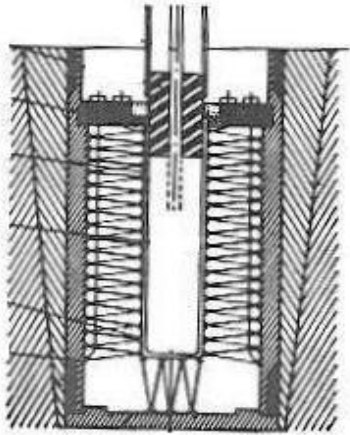
- ⌘ Active adiabatic calorimeters :
  - ⌘ Complicated set-up for immersion calorimetry-Never used
- ⌘ Passive adiabatic calorimeters (Zettlemoyer)
  - ⌘ Simple experiment. Most used in the past. Limited sensitivity
- ⌘ Passive diathermal with phase change (Chessick, liquid nitrogen)
  - ⌘ Delicate to operate, inaccurate
- ⌘ Passive diathermal with heat flowmeter (Tian-Calvet)
  - ⌘ Combines easy operation and high sensitivity. The most used to-day



# Features of the Tian-Calvet thermopile

400 to 2000 thermocouples :

- Integrate whole heat flow
- Convert heat-flow into voltage
- Provide high sensitivity
- Also provide high isothermicity
- When metallic, used between 77 to 1300 K



*Whith differential arrangement, Tian-Calvet thermopile suited for open system, with tubes, and compensates for heat leaks: well suited for adsorption studies*

# B/ Experimental procedures and derivation of thermodynamic quantities

1/ Gas adsorption calorimetry

2/ Immersion calorimetry



# 1/ Gas adsorption calorimetry

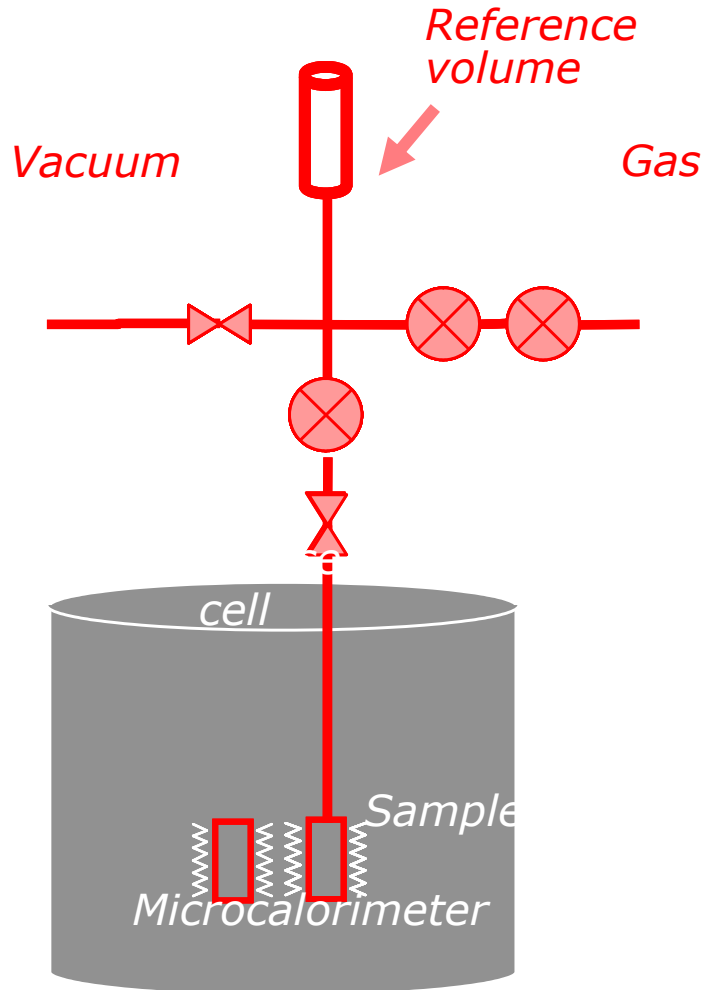
## Experimental procedures

- ⌘ Basic procedure: step by step introduction of the adsorptive
- ⌘ High resolution procedure
- ⌘ « Calorimetric weighing » procedure

## Assessment of thermodynamic functions

- ⌘ Simplified and accurate reporting of adsorption experiment: the Gibbs representation of surface excess quantities
- ⌘ Without calorimeter: the isosteric method
- ⌘ With the step-by-step procedure (open system, external work, reversibility requested for correct calculation and measurement)
- ⌘ With the high-resolution, quasi-equilibrium procedure

# The basic, point-by-point procedure for gas adsorption calorimetry



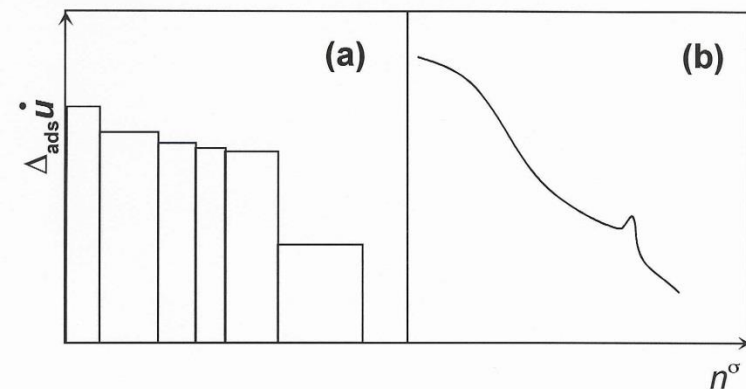
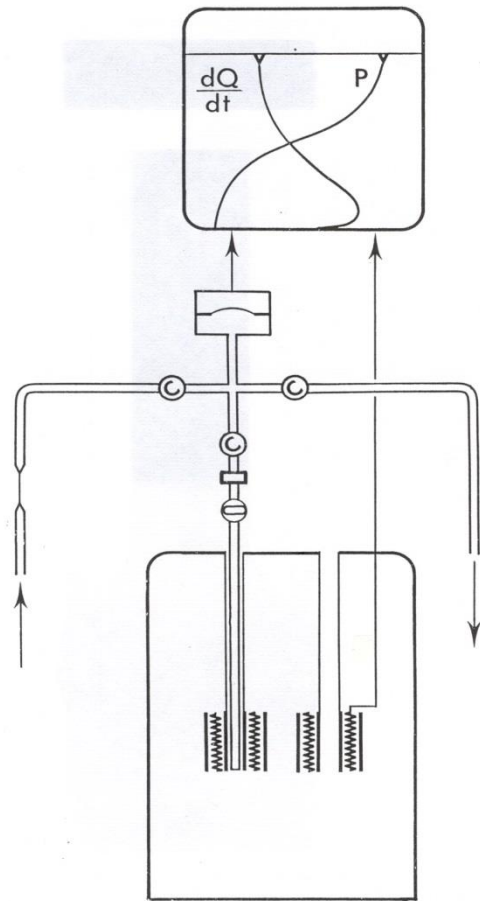
⌘ *Necessarily associates calorimetry with either adsorption manometry (usual) or adsorption gravimetry*

⌘ *Adsorptive must be introduced:*

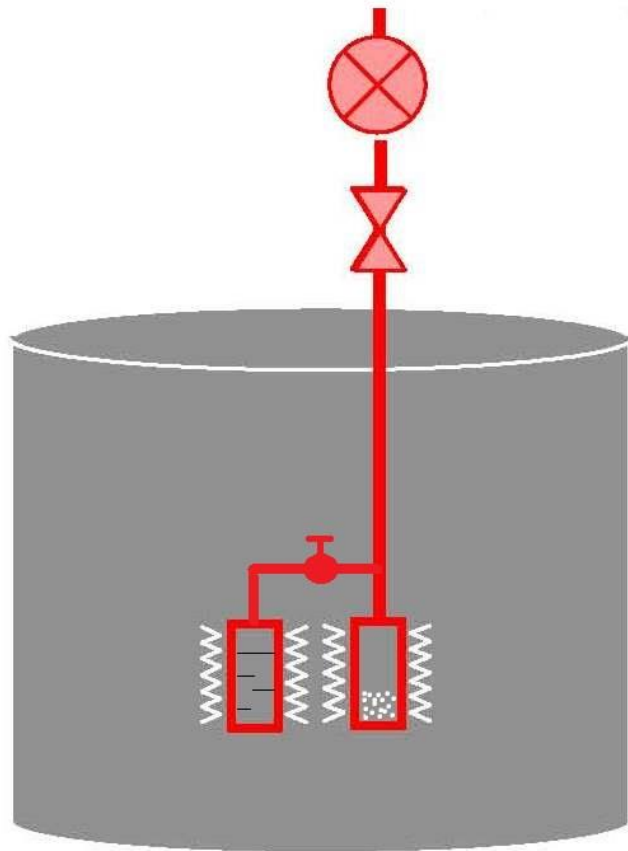
- ⌘ *slowly*
- ⌘ *at same  $T$  as calorimeter*

# The high-resolution procedure for gas adsorption calorimetry, with slow and continuous introduction of the adsorptive

- ⌘ A special device (sonic nozzle or gas-flow controller) allows *slow and continuous* introduction of adsorptive, at constant rate (ca 1 cm<sup>3</sup> STP/h)
- ⌘ Allows *direct recording of heat flow vs amount of adsorptive introduced*
- ⌘ Detects minute changes in mobility of adsorbate
- ⌘ Conveniently used up to 1 bar



# The procedure of adsorption calorimetry with Calvet's « calorimetric weighing »



- ⌘ *No need of external adsorption manometry or gravimetry*
- ⌘ *Associates 2 calorimeters in same thermostat*
- ⌘ *One to measure heat produced by adsorption*
- ⌘ *Another one to measure heat absorbed by liquid vaporizing towards adsorbent*
- ⌘ *Issue: spurious condensation, opening of valve produces noise in recording*
- ⌘ *Water condensation can be avoided by lowering  $p^\circ$  by salt*

# 1/ Gas adsorption calorimetry

## Experimental procedures

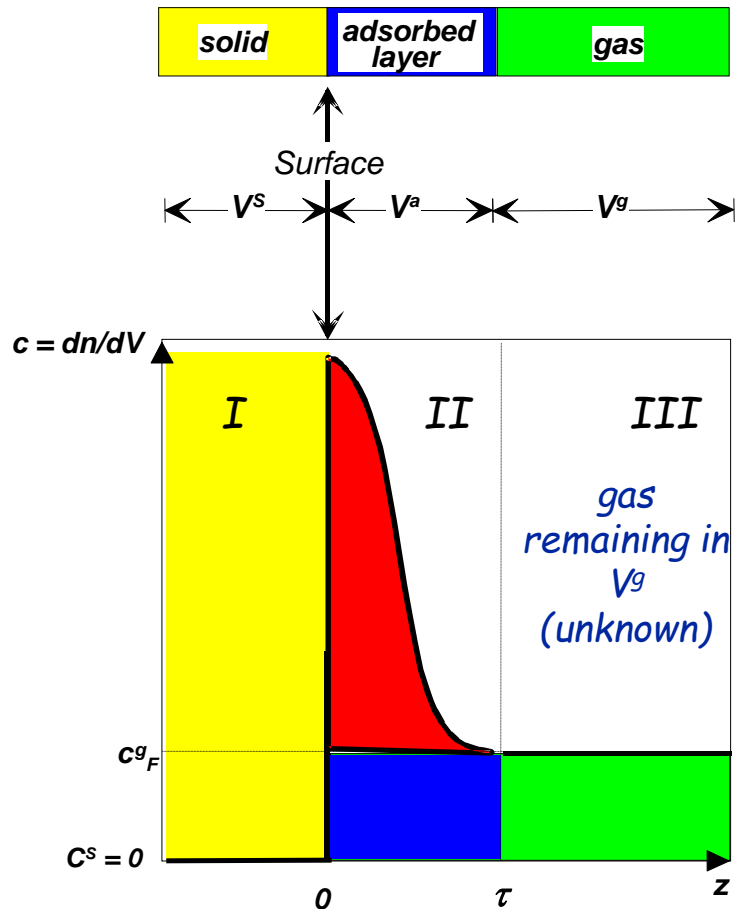
- ⌘ Basic procedure: step by step introduction of the adsorptive
- ⌘ High resolution procedure
- ⌘ « Calorimetric weighing » procedure

## Assessment of thermodynamic functions

- ⌘ Simplified and accurate reporting of adsorption experiment: the Gibbs representation of surface excess quantities
- ⌘ Without calorimeter: the isosteric method
- ⌘ With the step-by-step procedure (open system, external work, reversibility requested for correct calculation and measurement)
- ⌘ With the high-resolution, quasi-equilibrium procedure

# Two representations of adsorption equilibrium

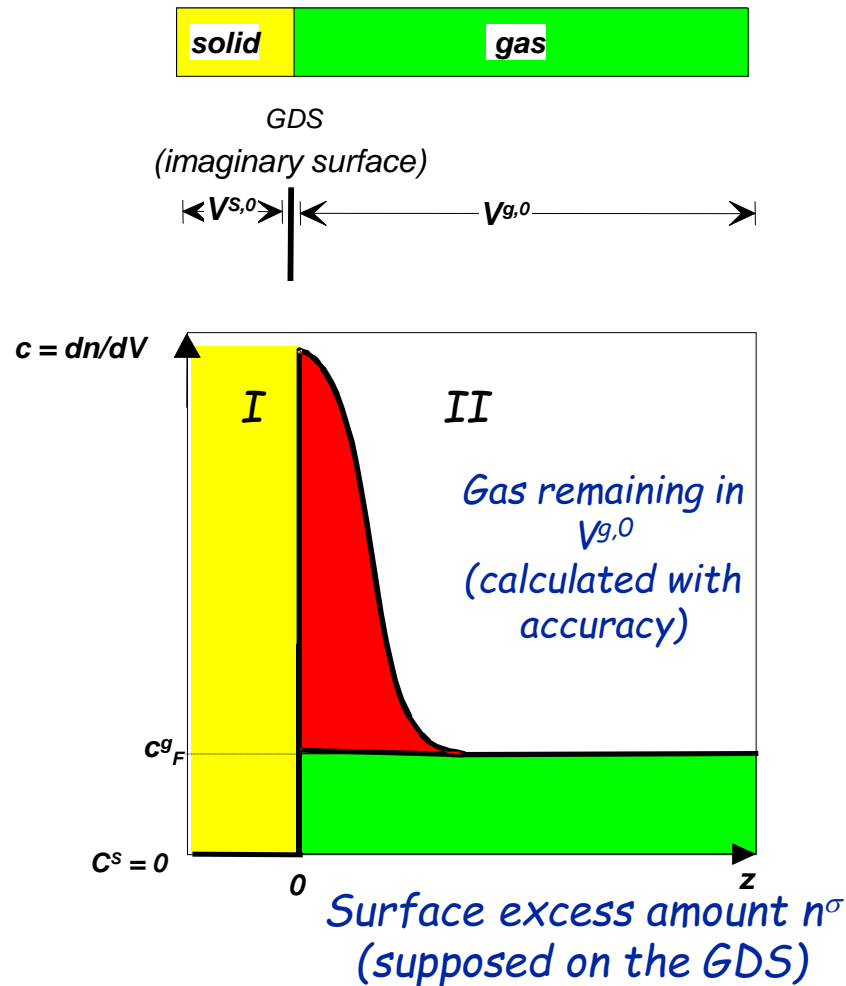
## Interfacial layer model



Adsorbed amount  $n^a$

$$n^a = A \int_0^{\tau} c \cdot dz$$

## Gibbs representation



$$n^\sigma = n_I^g - n_F^g$$

$$n^a = n^\sigma + c^g \cdot V^a$$

# Thermodynamics of adsorption in Gibbs representation

*Surface excess quantities (i.e. for a state)*

Surface excess energy  $U^\sigma = U - U^g - U^s$

Surface excess enthalpy

- After the usual definition of enthalpy  $H = U + pV$
- Since, in Gibbs representation  $V^\sigma = 0$  we get  $H^\sigma = U^\sigma$



# Thermodynamics of adsorption in Gibbs representation (continued)

Adsorption quantities (i.e. not for a state, for a change)

- Integral energy of adsorption (from 0 to  $n^\sigma$ )

$$\Delta_{ads}U = n^\sigma (\bar{u}^\sigma - u^g)$$

- Integral molar energy of adsorption (from 0 to  $n^\sigma$ )

$$\Delta_{ads}\bar{u} = \Delta_{ads}U / n^\sigma = \bar{u}^\sigma - u^g$$

- Differential (derivative) energy of adsorption

$$\Delta_{ads}\dot{u} = \frac{dU}{dn^\sigma} = \dot{u}^\sigma - u^g$$

- Differential (derivative) enthalpy of adsorption

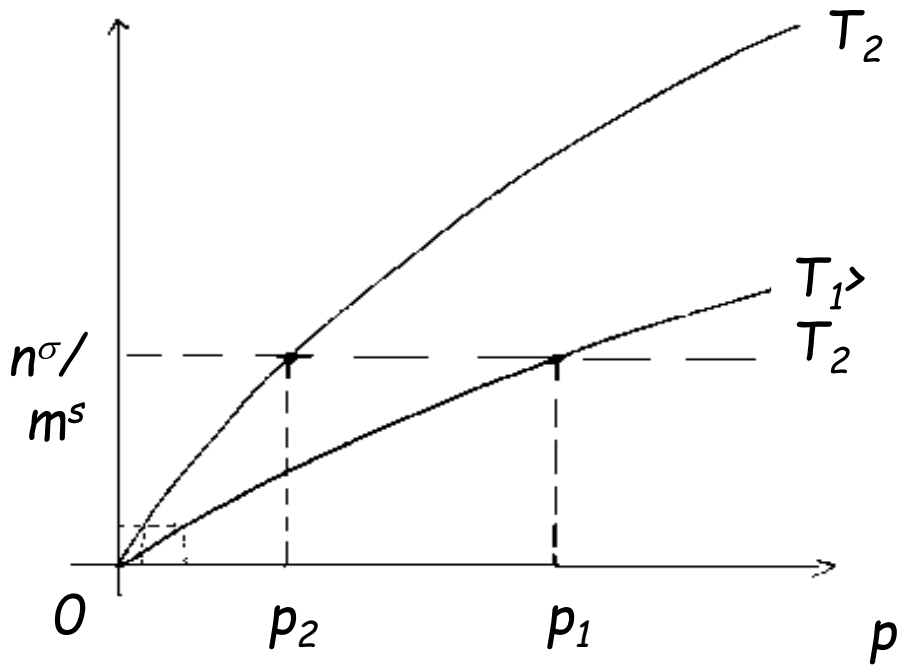
$$\Delta_{ads}\dot{h} = \frac{dH}{dn^\sigma} = \dot{u}^\sigma - h^g = \dot{u}^\sigma - u^g - RT$$

- Isosteric enthalpy (heat)  $q_{st} = -\Delta_{ads}\dot{h}$



# The isosteric method

« Isosteric » i.e. for same « volume » adsorbed



$$Q_{st} = R T_1 T_2 / (T_2 - T_1) \ln (p_2 / p_1)$$

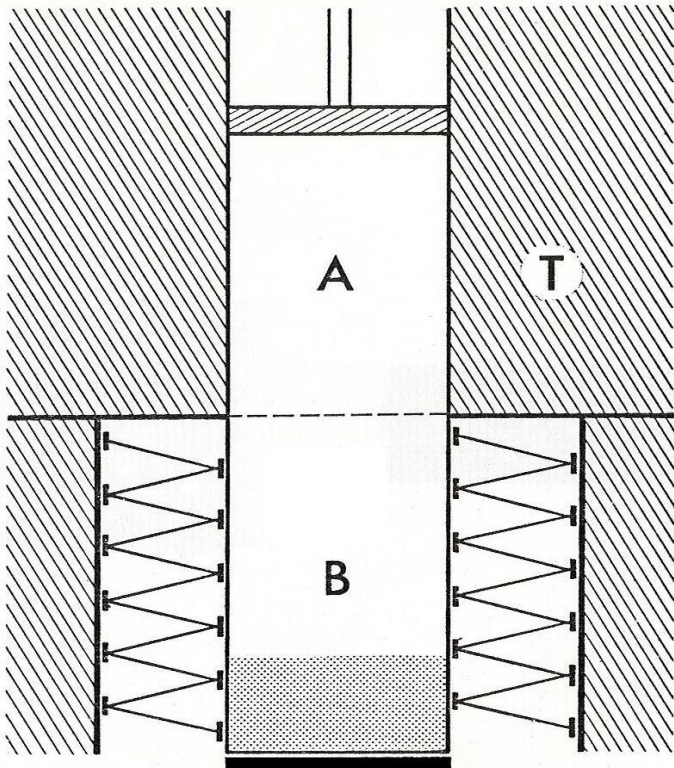
$$\Delta_{ads} \dot{h} = - R T_1 T_2 / (T_2 - T_1) \ln (p_2 / p_1)$$

One can easily replace the term « isosteric heat » by the more explicit term « isosteric enthalpy ».

This makes easier the connection and comparison with enthalpies obtained by calorimetry

# Open system: point by point gas adsorption calorimetry

*To reach an adsorption enthalpy, how can we take into account the fact that the system is open?*



*(Rouquerol and Everett, 1985)*

- Imagine all adsorptive in a cylinder, partly in calorimeter
- Assume reversible compression by slowly depressing the piston
- Calculate the heat of compression evenly dissipated to the surroundings at constant  $T$
- Take into account that calorimetric cell B only dissipates part of the total heat of compression

# Open system: point by point gas adsorption calorimetry

Interest of « isothermal » calorimetry :

→  $T$  of the adsorption system remains constant

Association with adsorption manometry :

→ The adsorption system is an open system

Calculation of compression work due to gas entrance

(possible check by blank experiment) :

Gas should be introduced slowly enough to ensure reversibility, so that:  $dW = V_c dp$

For open system, 1<sup>st</sup> principle of thermodynamics tells :

- $dU = dW_{T,V} + dQ_{T,V} + u^g (dn^g + dn^o)$

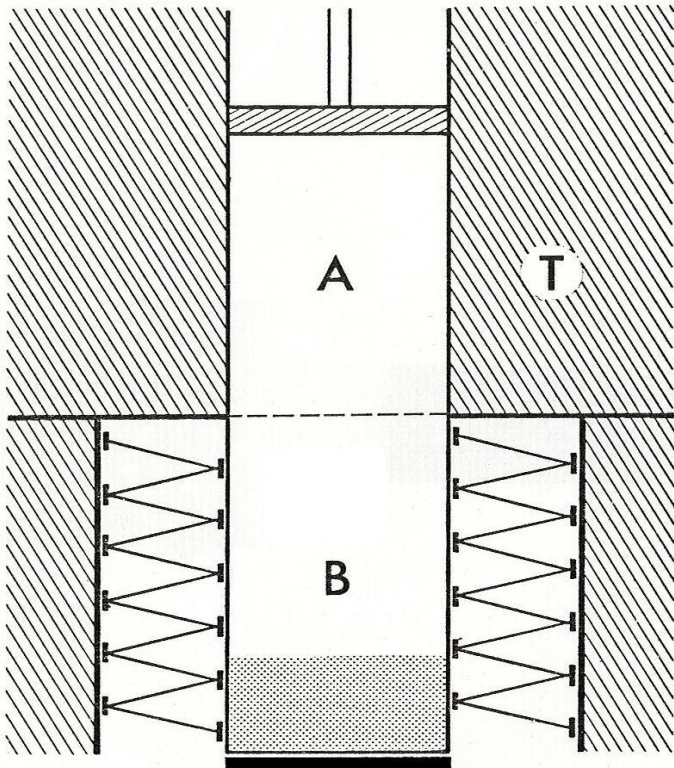
- $dW = V_c dp + RT dn^o$

$$\frac{dQ}{dn^o} + V_c \frac{dp}{dn^o} = \left[ \frac{dU}{dn^o} - u^g RT \right] = \Delta_{ads} h_{T,P}$$



# Open system: point by point gas adsorption calorimetry

*Conditions to satisfactorily assess an enthalpy of adsorption :*



*(Rouquerol and Everett, 1985)*

- Well-defined starting state (careful outgassing)
- Consider operation in open system
- Introduce adsorptive reversibly
- Calculate heat of compression
- End with differential enthalpy of adsorption (and not with « heat », which depends on calorimeter and procedure)

# 1/ Immersion calorimetry

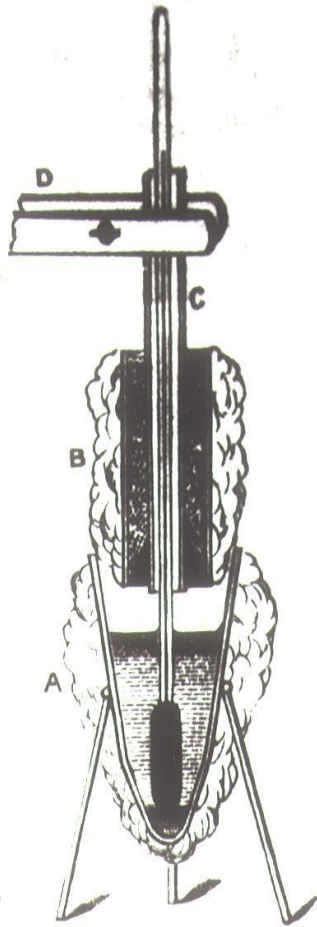
## Experimental procedures

- ⌘ First experiment: Pouillet: dry adsorbent falls into water
- ⌘ Up to 1975: glass bulb broken (up to 2 J!)
- ⌘ Then many trials to lower this irreproducible effect
- ⌘ Still to-day, glass bulb, with brittle end, the safest. Limits extension of immersion calorimetry
- ⌘ Finally, recommended procedure

## Assessment of thermodynamic functions

- ⌘ Need of well-defined starting and final states (hence glass bulb!)
- ⌘ Needs corrections; achieves good reproducibility
- ⌘ The enthalpy of immersion can be compared with the enthalpy of adsorption

# Various forms of Immersion Calorimetry

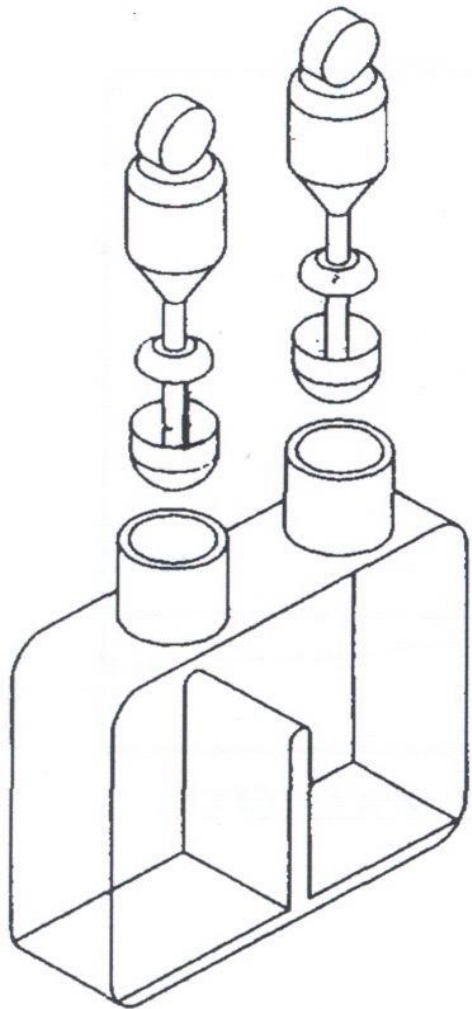


z Claude Pouillet 's experiment (1822)  
Dry sand flows from black cylinder down to water enclosed in glass vessel, wool-insulated  
Thermometer reads increase of ca 2 K. ( $\pm 30\%$ )

z A.C.Zettlemoyer (1950-1970) made use of a «water » or « isoperibol » calorimeter  
with glass spherical bulb to  
be broken

Interest of glass bulb: well-defined starting state  
Limitation: heat of breakage up to 1 J ( $\pm 5-10\%$ )

# Various forms of Immersion Calorimetry



z J.Rouquerol and J.Van der Deelen (1971) and C.Moreno-Pirajan *et al.*(1996) made use of a **revolving cell** with partial separation (cf drawing)

Interest: most easy to use

Limitation: starting sample in the presence of vapour

z J.Rouquerol and S.Partyka (1974) separated liquid and solid by thin **metal foil** with O-ring, to be pierced by a lancet

Interest: easy to use, no glass blowing

Limitation: not as tight as a glass bulb

z Finally, J.Rouquerol and S.Partyka (1975) proposed procedure which successfully:

- lowers value of corrective terms

- reaches enthalpy change, not only heat ( $\pm 1-2\%$ )



# 1/ Immersion calorimetry

## Experimental procedures

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# Multiple origins of heat effect in immersion experiment

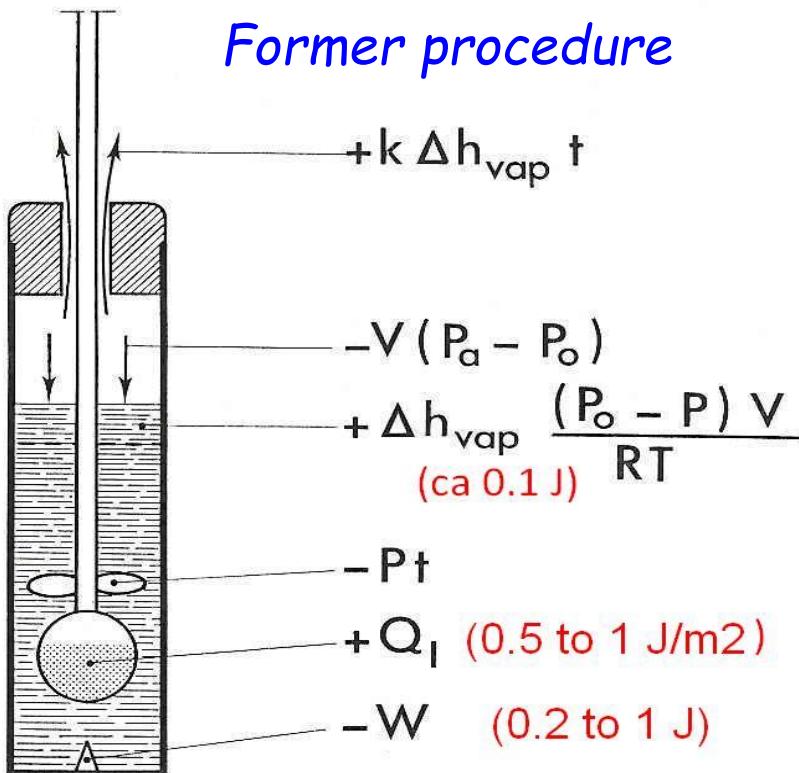
$$Q_{\text{measured}} = \Delta_{\text{imm}} U \text{ immersion energy (0.5 to 1 J.m}^{-2}\text{)}$$

✦  $W_b$  ampoule *breaking* (0.2 to 1J, if spherical bulb)

✦ *work of atmospheric pressure* on depression of liquid level, when filling void volume of bulb

✦ *energy of vaporization* (around 0.1 J)

Conclusion: need to reduce and control corrective terms in order to only assess meaningful  $\Delta_{\text{imm}} U$



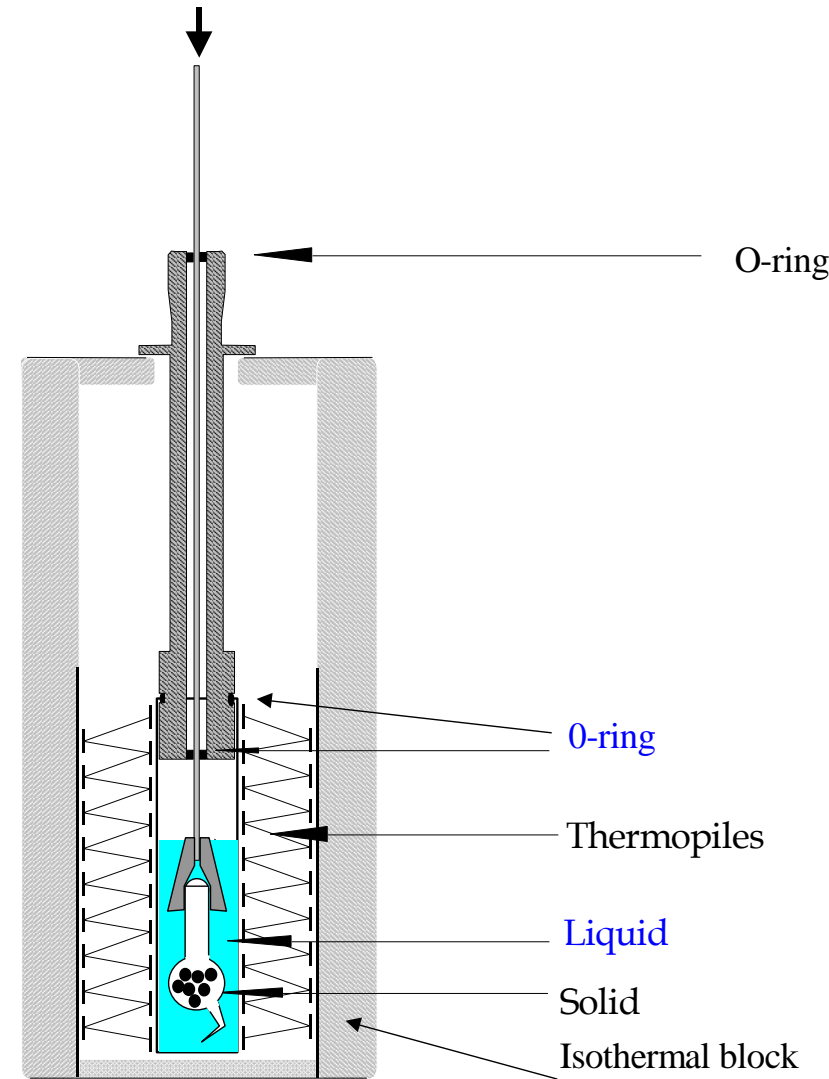
# Strict procedures to assess state function in immersion calorimetry (Rouquerol and Partyka, 1975)

Makes use of:

- Tian-Calvet differential microcalorimeter (passive diathermal)
- Sealed bulb (keeps sample outgassed)
- Fragile brittle end (reduces heat to 5-10 mJ)
- Tight system (O-ring) to prevent evaporation and avoid work of atmospheric pressure
- O-ring out of calorimeter to avoid heat of friction to be measured

Requests:

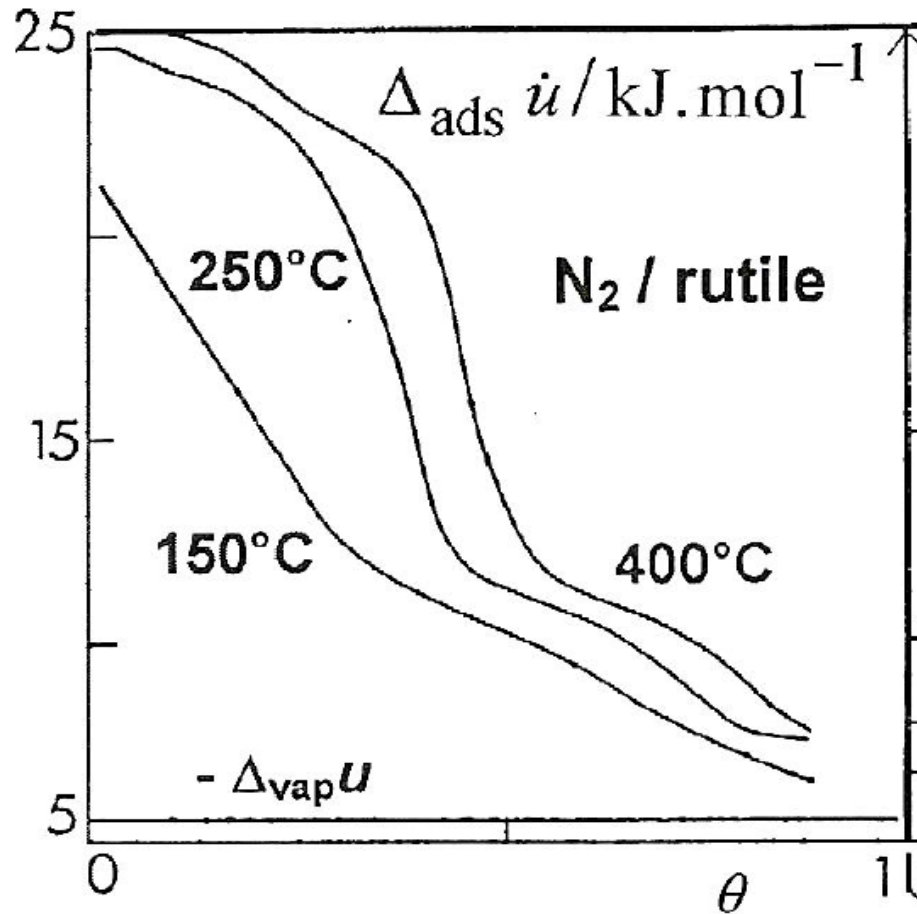
- Glass-blowing to make the bulb
- Careful sample outgassing (by Controlled Rate Thermal Analysis when possible)
- Sealing
- Evaluate all corrections to assess a  $\Delta_{imm}H$



## C/ Three applications of gas adsorption calorimetry

- 1/ Evaluation of the validity of the BET model
- 2/ Detection of mobility or phase changes
- 3/ Study of deformation of adsorbents

# BET assumes $\Delta_{\text{ads}}H$ constant during completion of monolayer

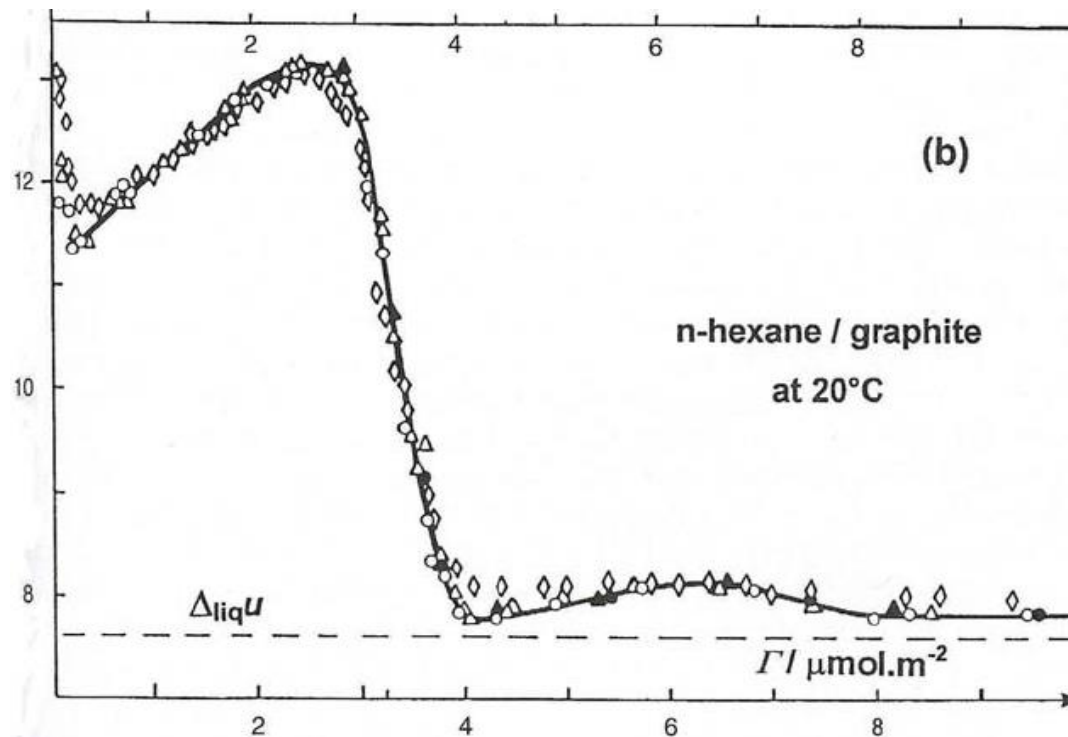


*Direct calorimetric measurements show that, even in the absence of microporosity,  $\Delta_{\text{ads}}U$  varies much, even with argon, as soon as « active sites » are on the surface (here, hydroxyls and  $\text{Ti}^{+++}$  cations)*

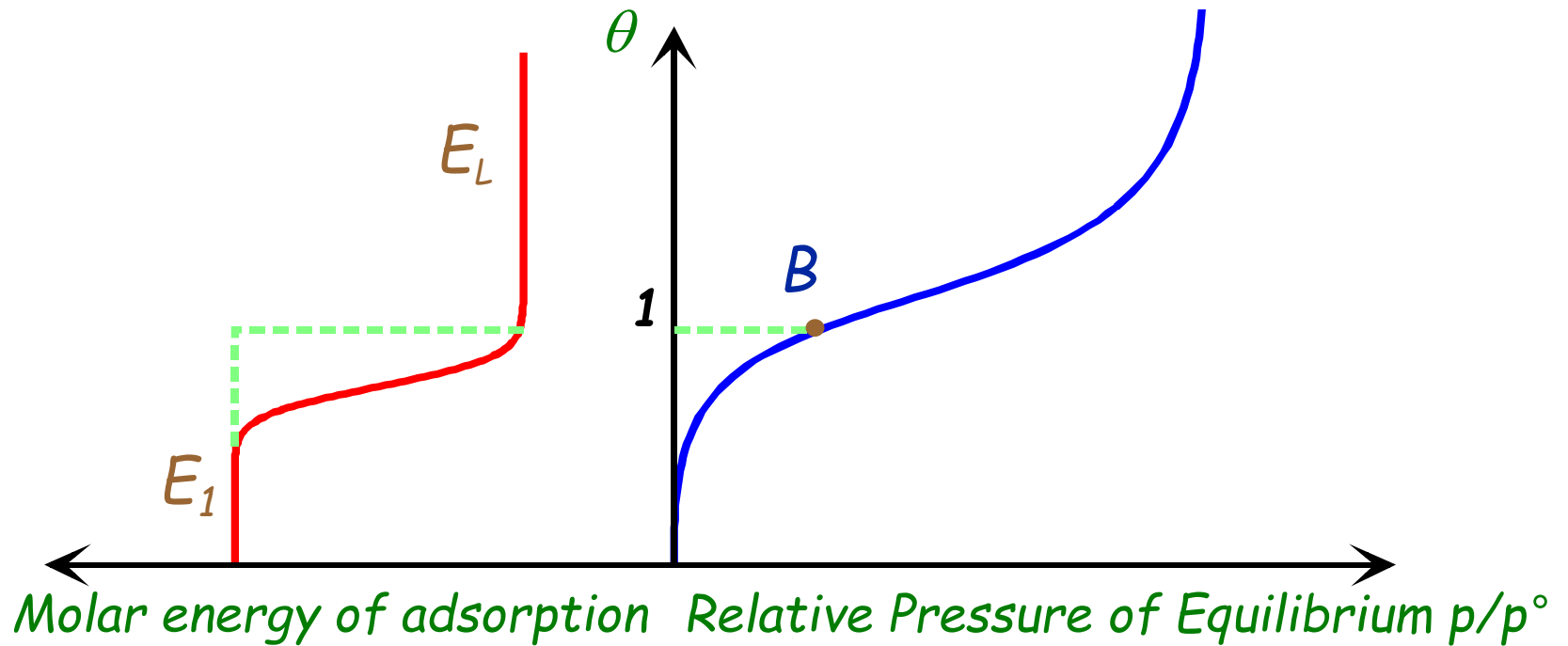
# BET assumes no "lateral interactions" during formation of 1st layer

*Calorimetry clearly shows increased interaction between N-hexane molecules during formation of monolayer*

*(A.A.Isirikian and A.V.Kiselev,1962)*



BET assumes multilayer starts before monolayer is completed (correct)



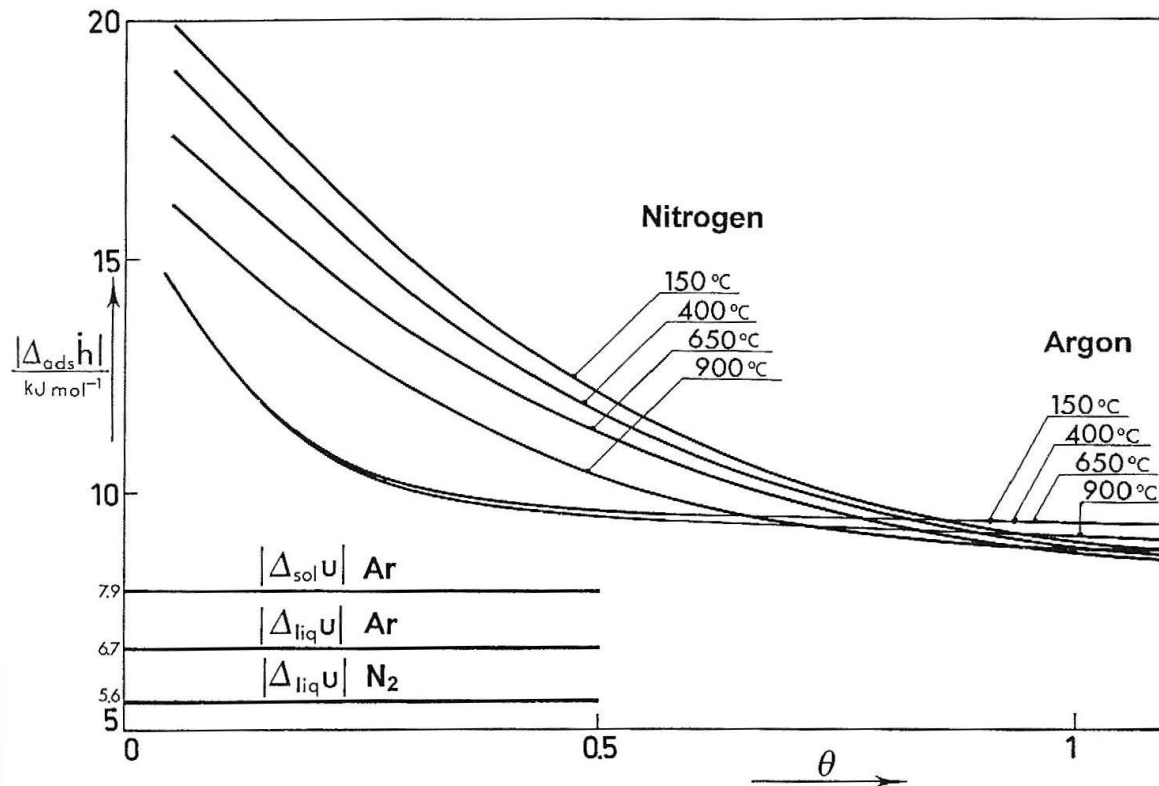
$E_1$  = Molar energy of adsorption for the first adsorbate layer

$E_l$  = Molar energy of liquefaction of the adsorptive at the temperature of adsorption



BET assumes  $N_2$  molecule takes any orientation in the monolayer

Calorimetric study of  $N_2$  interaction with hydroxyls on silica surface



➤ For Ar, no effect of concentration of OH groups

➤ For  $N_2$ ,  $\Delta_{ads} H$  increases by 3kJ from bare to fully hydroxylated surface

➤ Enough to explain orientation of  $N_2$  molecule on surface

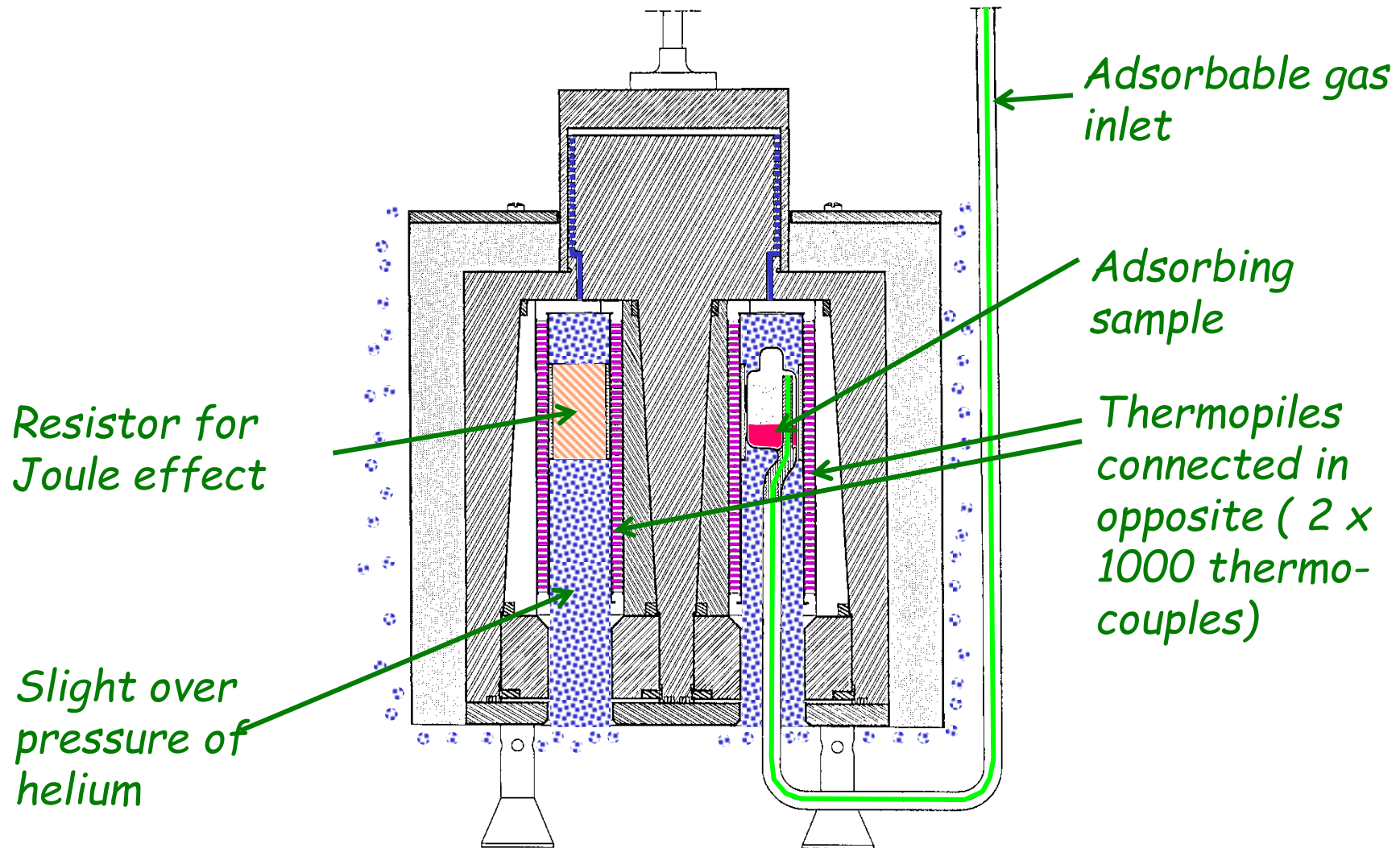
## C/ Three applications of gas adsorption calorimetry

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# Adsorption calorimetry at liquid $N_2$ or Ar temperature



# The Gas Adsorption Calorimeter in its Liquid Cryostat

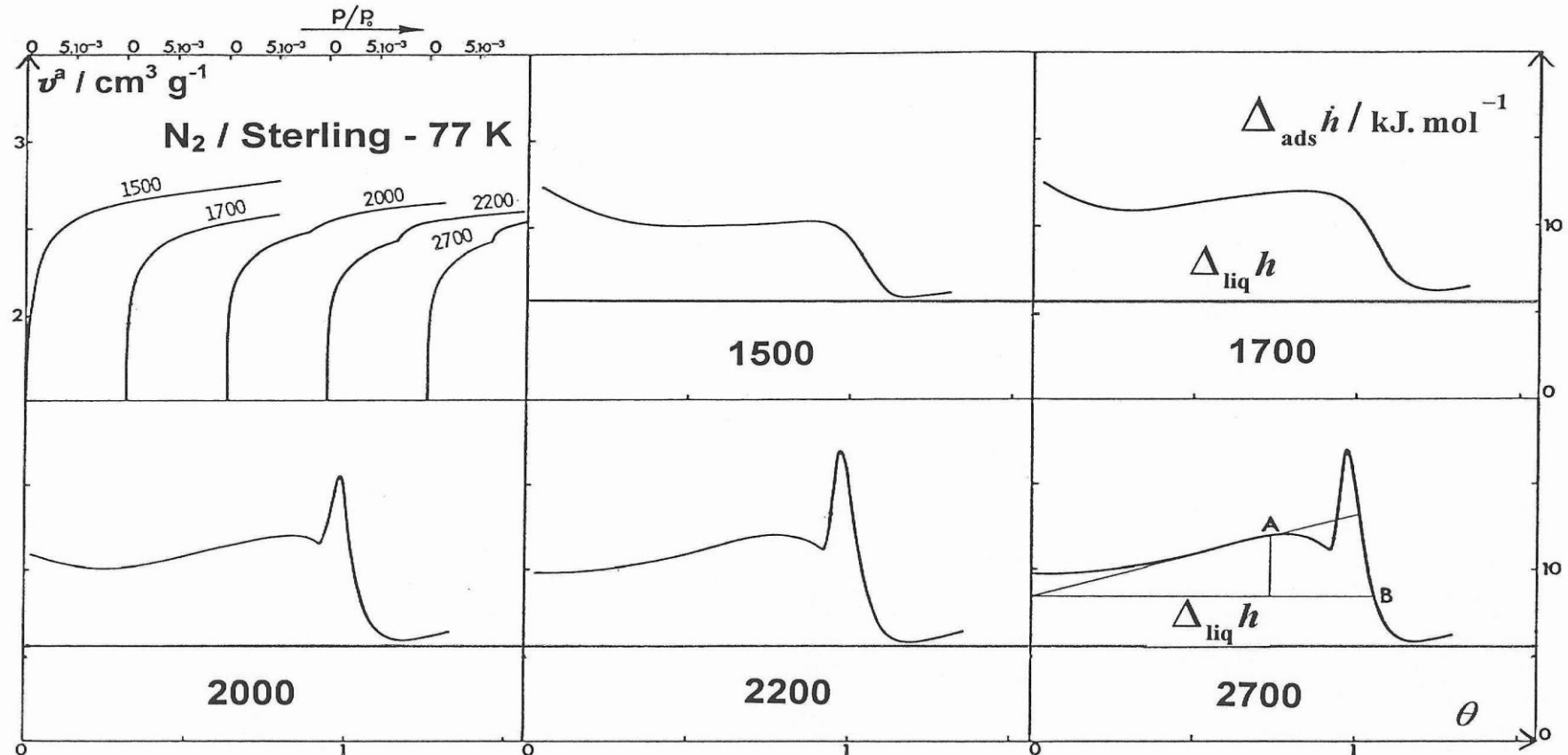


*Helium gas (flow rate  $1 \text{ ml.mn}^{-1}$ ) carefully cooled in « aluminum tower » (3 m cooling path).*

*Completely immersed in either liquid nitrogen or liquid argon*



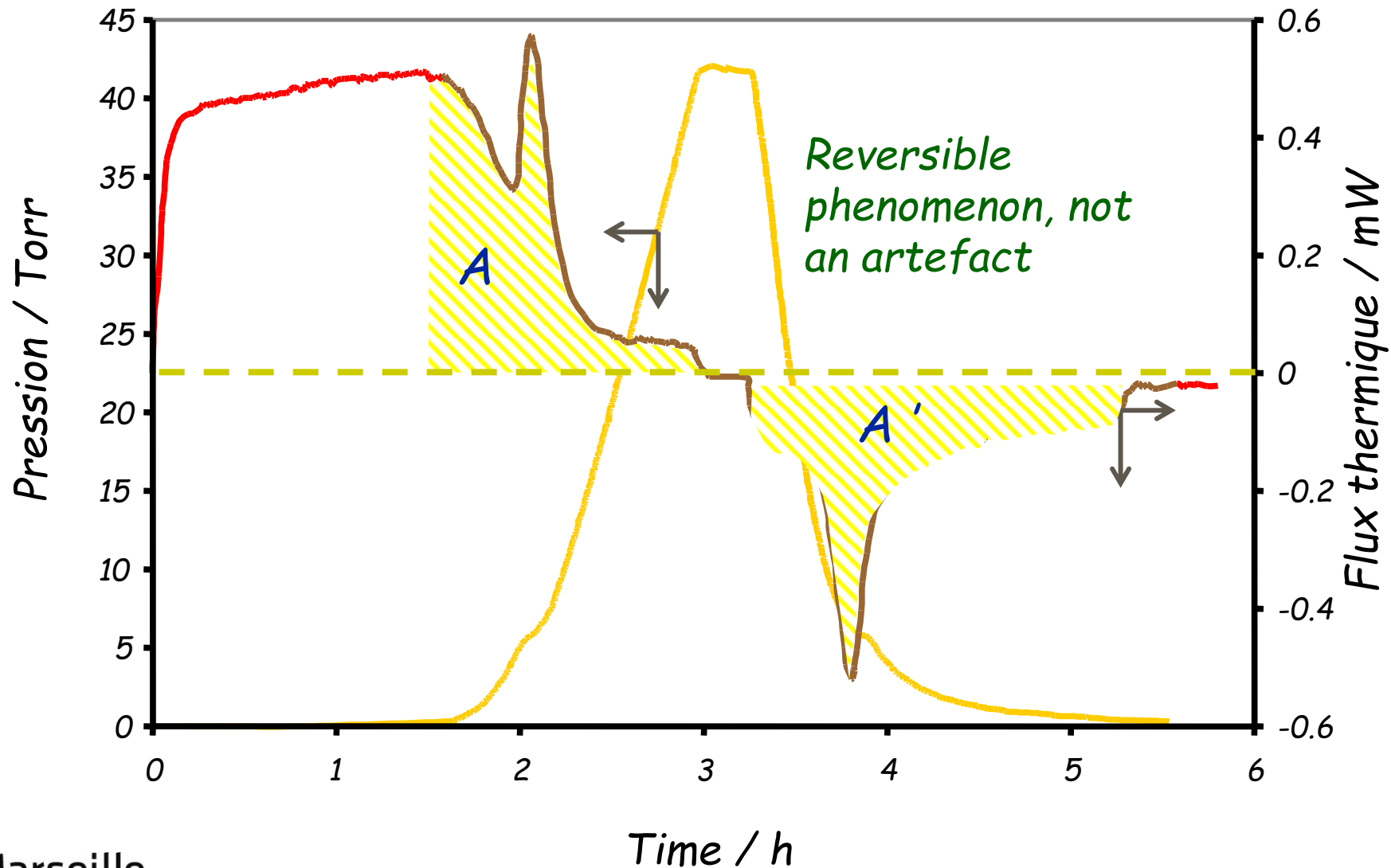
Adsorption calorimetry of  $N_2$  on carbon black at 77 K :  
 as graphitization  $T$  increases, exothermic peak (and substep) more and more visible at completion of monolayer



z Is it an artefact due to quasi-equilibrium procedure ?

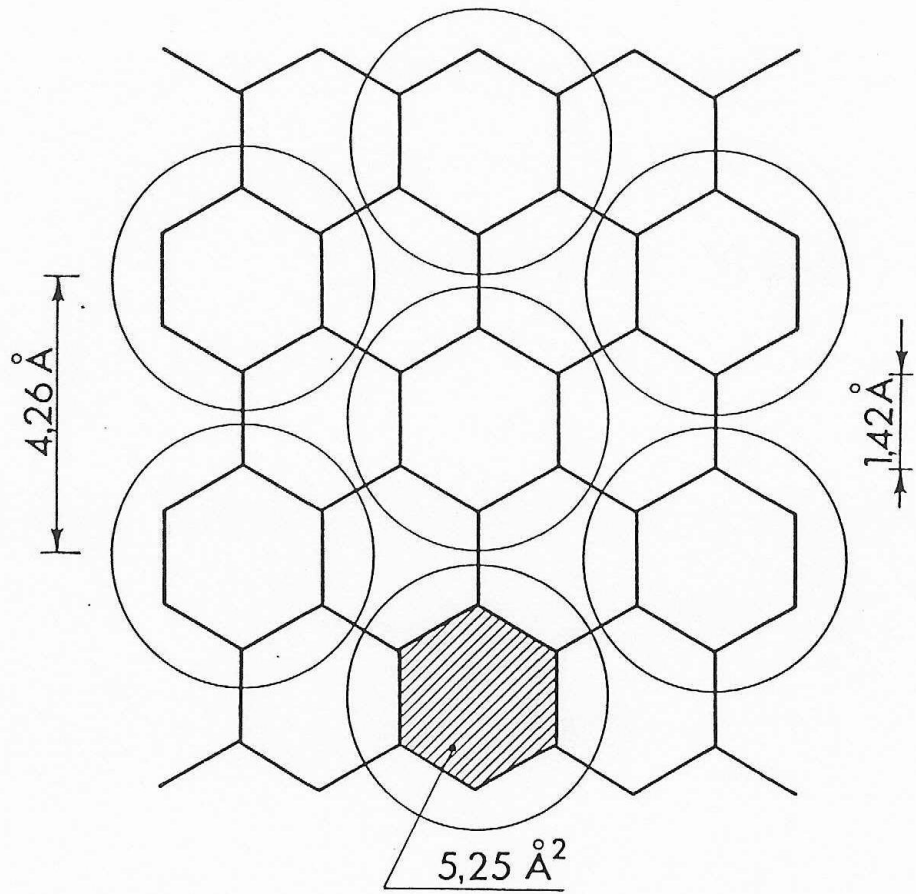


$N_2$  / Graphite at 77 K: exothermic peak on adsorption, endothermic on desorption

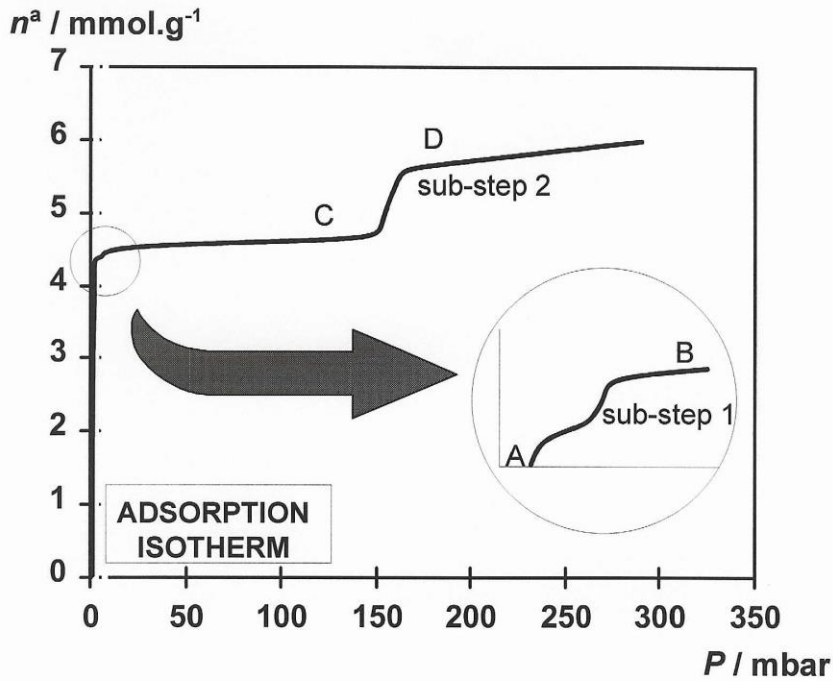




# Explanation of exothermal peak at completion of N<sub>2</sub> monolayer on graphite



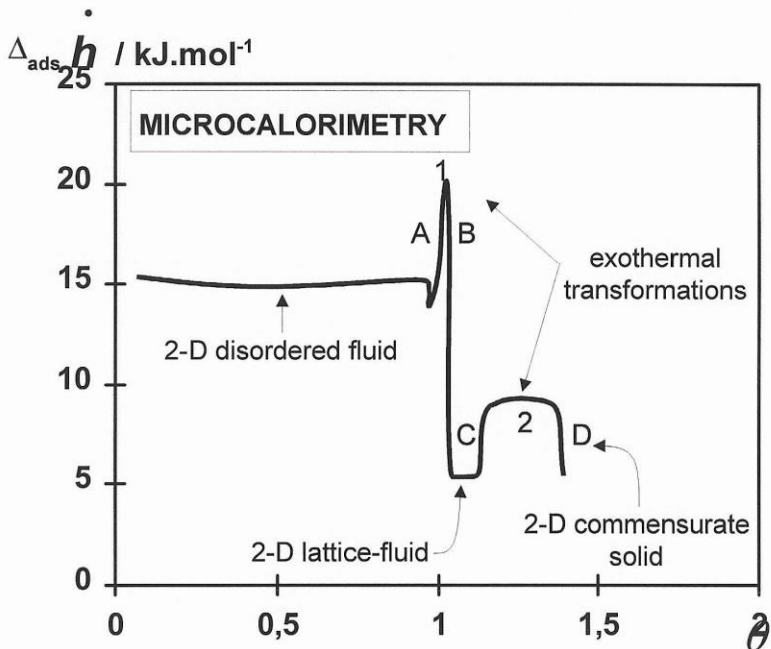
- z Neutron diffraction shows epitaxial superstructure appearing during occurrence of peak
- z Just as if we had sudden freezing of monolayer
- z Diffraction parameters correspond to 1 N<sub>2</sub> over 3 graphitic rings ie 15.75 Å<sup>2</sup>
- z Hence a precise mode of determination of the surface area of graphite



## Nitrogen on Silicalite at 77 K

(P.Llewellyn et al., 1993)

- z On adsorption isotherm: 2 substeps
- z On curve of differential enthalpy of adsorption: 2 exothermal peaks, for same coverage as substeps
- z Neutron diffraction shows peaks correspond to changes in mobility and localisation



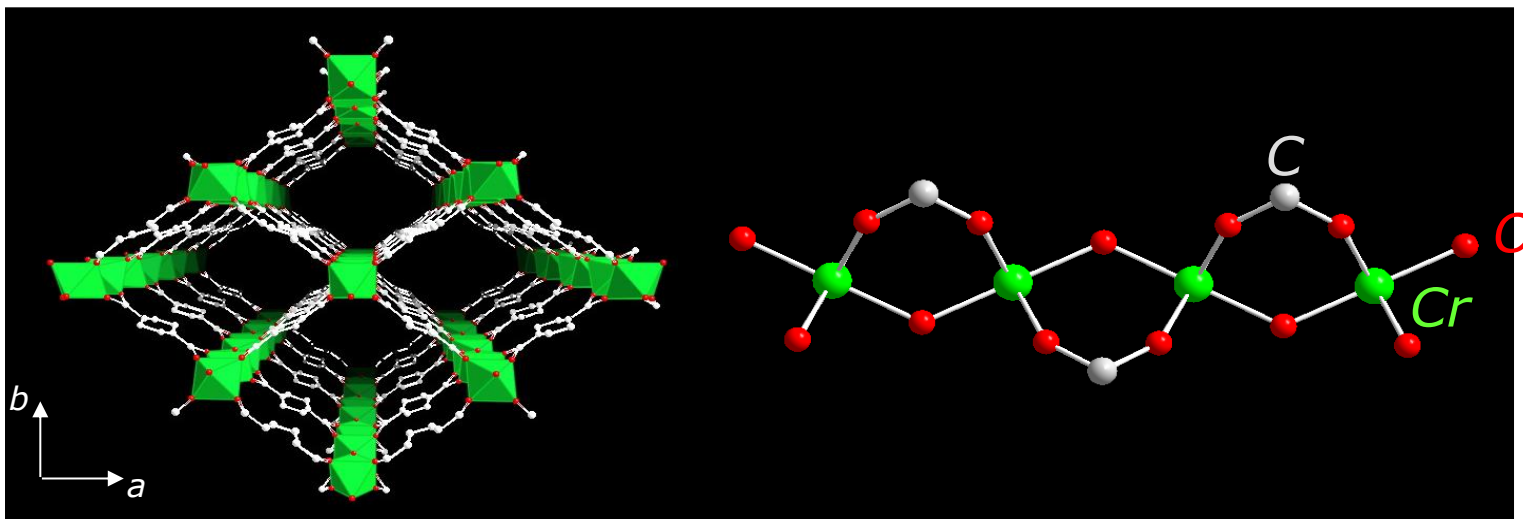
## C/ Three applications of gas adsorption calorimetry

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## MOF MIL-53 (Cr) : Chromium 1,4-benzenedicarboxylate

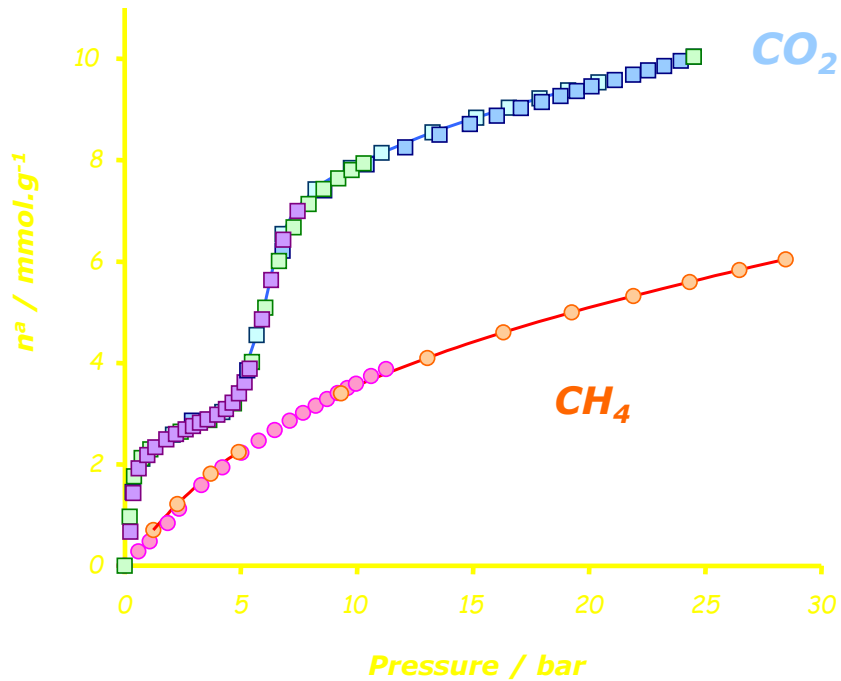


- ✓ Chains of corner-sharing  $\text{CrO}_4(\text{OH})_2$  octahedra interconnected by dicarboxylate groups
- ✓ Nanoporous open-framework with empty pores of width  $\sim 0.8$  nm
- ✓ Stable up to  $300^\circ\text{C}$  in air

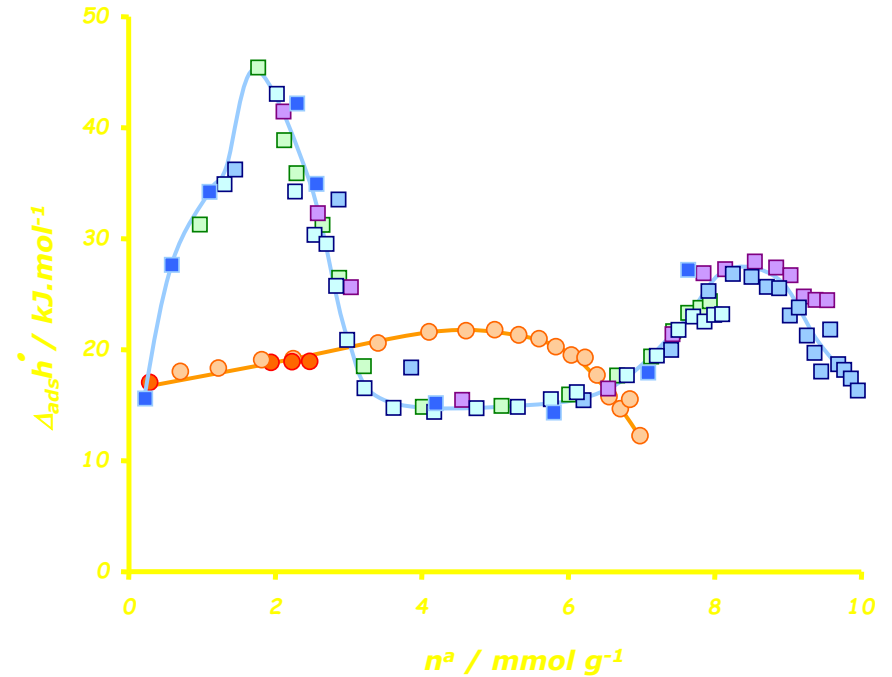
G.Ferey et al., *J.Amer.Chem.Soc.*, 2002

# CO<sub>2</sub> vs. CH<sub>4</sub> on (Cr)MIL-53 @ 304K

## Isotherms



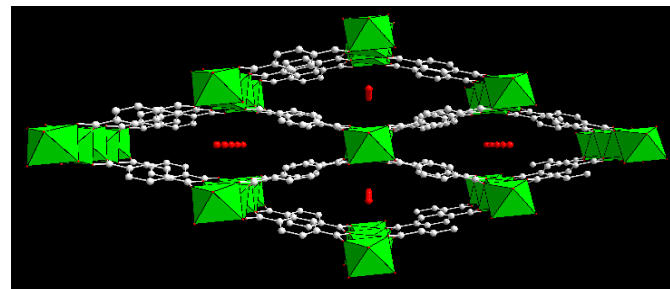
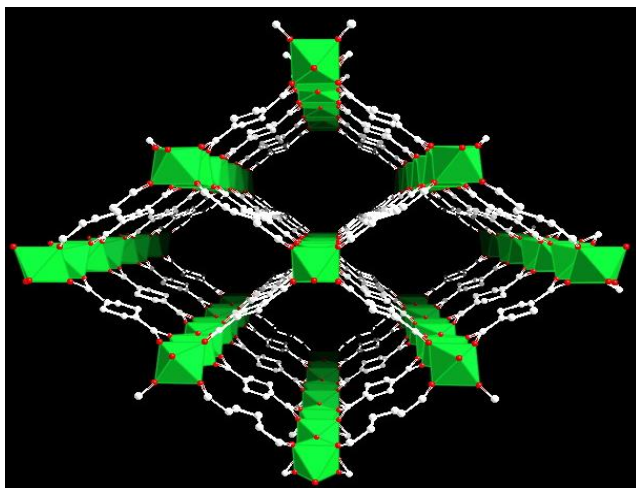
## Enthalpies of adsorption



Explanation: step (isotherm) and peak (enthalpies) correspond to enhanced interaction of CO<sub>2</sub> with more compact porous framework. Why?

*On MIL-53 (Cr),  
a breathing phenomenon occurs with CO<sub>2</sub>, like for H<sub>2</sub>O*

*Adsorption-desorption process is accompanied by a reversible  
breathing effect and shrinkage of the pores*



*Confirmed by synchrotron XRD (structure change) and  
FTIR (interaction change)*

*(P.Llewellyn and S.Bourelly,,2008,, submitted to publication)*



## D/ Three applications of immersion calorimetry

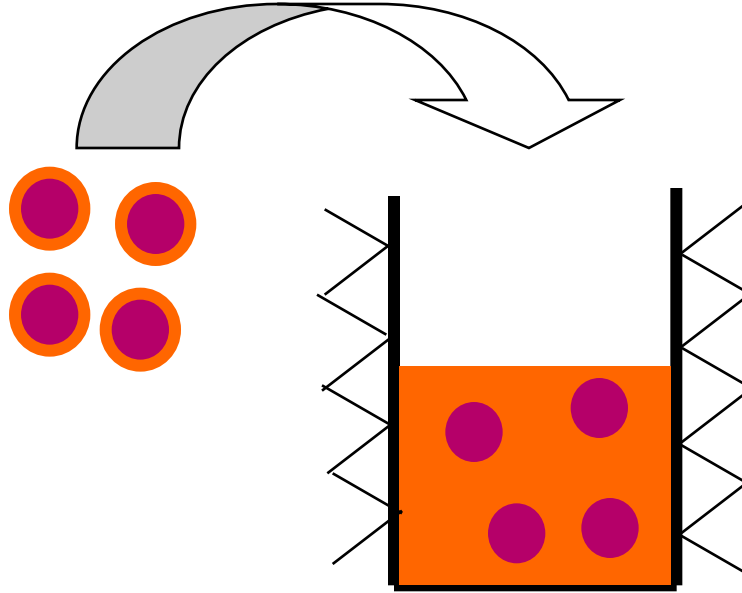
1/ Determination of the non-microporous surface area of adsorbents by the modified Harkins and Jura calorimetric method

2/ The determination of the overall surface area (including microporous) of activated carbons

3/ The "screening" with immersion liquids of different molecular sizes to determine a micropore size distribution or a separation ability

# Modified Harkins and Jura's « absolute » method for the determination of the specific surface area of non- porous powders

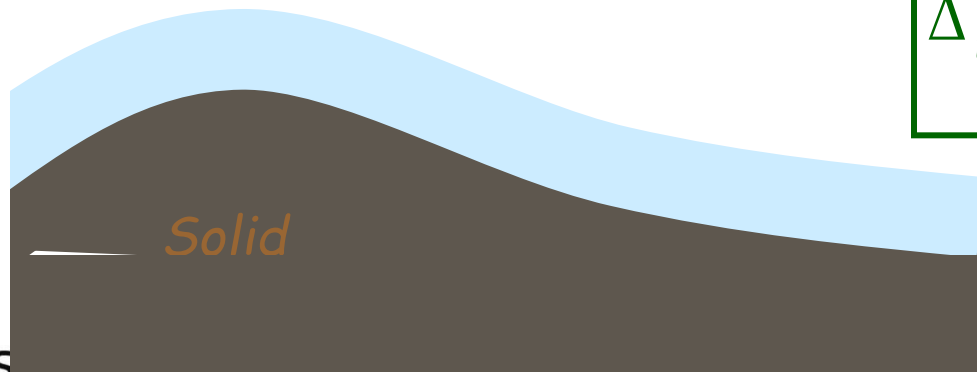
1/ Pre-cover  
powder with only 2  
layers of water



2/ Immerse in water in  
calorimeter

Disappearance of the  
water/vapour interface

Liquid film, thick enough  
to screen high energy sites



$$\Delta_{imm} U = A \cdot \left( \gamma_{lv} - T \cdot \left( \frac{\partial \gamma_{lv}}{\partial T} \right)_A \right)$$

$\gamma_{lv}$

## *Specific surface area: comparing the modified Harkins and Jura immersion calorimetric method with the BET (N<sub>2</sub>)*

| <b>Powder</b>            | <b>Harkins-Jura</b> | <b>BET</b>  |
|--------------------------|---------------------|-------------|
| <b>Aerosil</b>           | <b>140</b>          | <b>129</b>  |
| <b>Alumina</b>           | <b>100</b>          | <b>81</b>   |
| <b>Titania</b>           | <b>63</b>           | <b>57</b>   |
| <b>Gallium Hydroxide</b> | <b>21.3</b>         | <b>21</b>   |
| <b>Kaolin A</b>          | <b>19.4</b>         | <b>19.3</b> |
| <b>Kaolin B</b>          | <b>19.2</b>         | <b>12.1</b> |
| <b>Quartz</b>            | <b>4.2</b>          | <b>4.3</b>  |
| <b>Zinc Oxide</b>        | <b>3.1</b>          | <b>2.9</b>  |
| <b>Calcite</b>           | <b>0.8</b>          | <b>0.6</b>  |
| <b>Gibbsite</b>          | <b>27</b>           | <b>24</b>   |

### *Advantages:*

- no assumption about cross section of adsorbed molecule*
- interesting reference method*

### *Limitations:*

- requests full wetting of material*
- time consuming experiment*
- only assesses « external » area (non-microporous) like the BET*
- but this limitation is solved by another calorimetric method*

## D/Three applications of immersion calorimetry

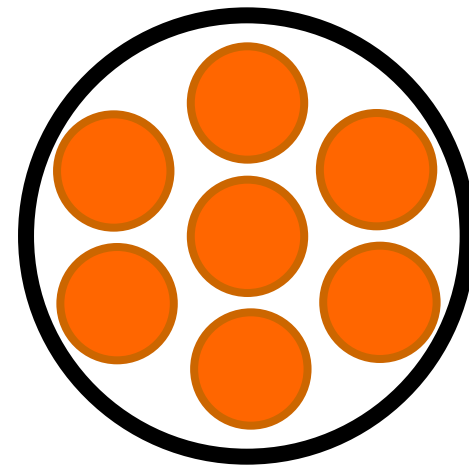
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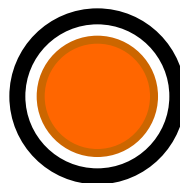
3/ The "screening" with immersion liquids of different molecular sizes to determine a micropore size distribution or a separation ability

For microporous materials, weakness of BET assumption that area  $\sigma$  covered by a molecule is constant

$$\sigma = 0,85$$

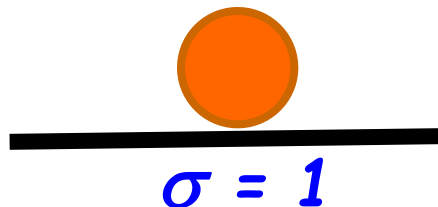


$$\sigma = 4$$



In cylindrical pores

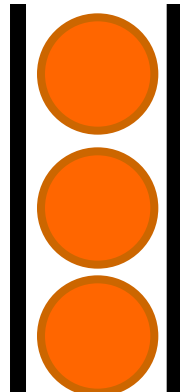
On flat surface, as always assumed by BET



$$\sigma = 1$$

$\sigma$  is the area covered per molecule

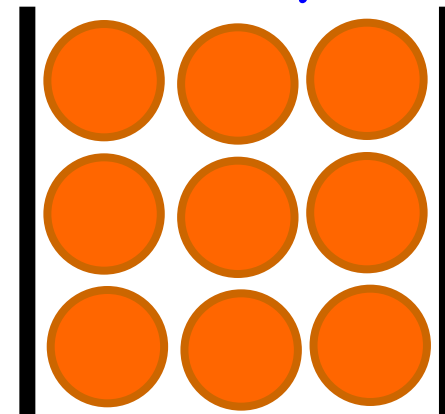
$$\sigma = 2$$



In slit-shaped pores

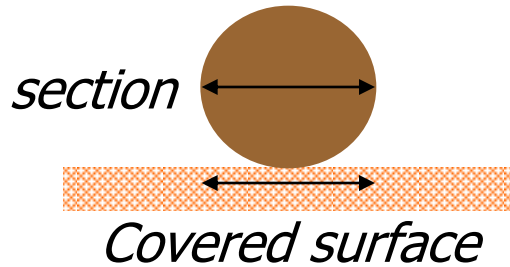
Ultramicropores  
BET underestimates

$$\sigma = 0,6$$

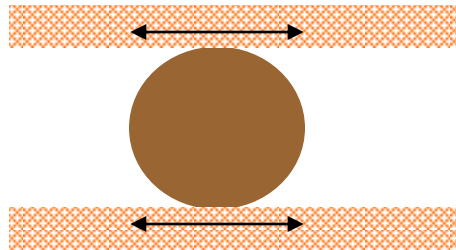


Supermicropores  
BET overestimates

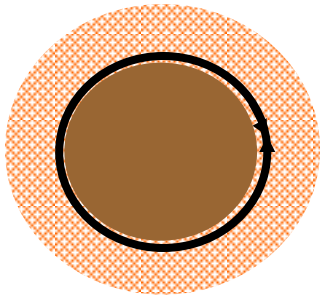
# The adsorption potential is proportional to the area covered by one molecule adsorbed



Non porous surface  $a_{\text{BET}}=a_{\text{real}}$   
Covered surface = 1 molecular cross section  
Interaction energy 1  $U^\circ$



Slit-shaped micropore:  $a_{\text{BET}}=a_{\text{real}}/2$   
Covered surface= 2 molecular cross sections  
Interaction energy  $U=2 U^\circ$



Cylindrical micropore :  $a_{\text{BET}}=a_{\text{real}}/4$   
Covered surface= 4 molecular cross sections  
Interaction energy  $U=4 U^\circ$

( Interaction energies calculated from dispersion forces, Everett and Powl,1976)



# For the assessment of the surface area of microporous materials, how calorimetry can help?

- ⌘ Calorimetry is sensitive to the interaction energy
- ⌘ Now, the adsorption potential is proportional to the area covered by one molecule adsorbed
- ⌘ Therefore, the energy of immersion is proportional to the area, even for microporous materials

Hence derivation of surface area  $a_{imm}$  accessible by immersion calorimetry in non-polar liquids (non specific interaction, mainly dispersion forces)

$$a_{imm} = \frac{\Delta_{imm}H(\text{sample}) / J g^{-1}}{\Delta_{imm}H(\text{ref}) / J g^{-1}} \cdot a_{BET}(\text{ref}) / m^2 g^{-1}$$

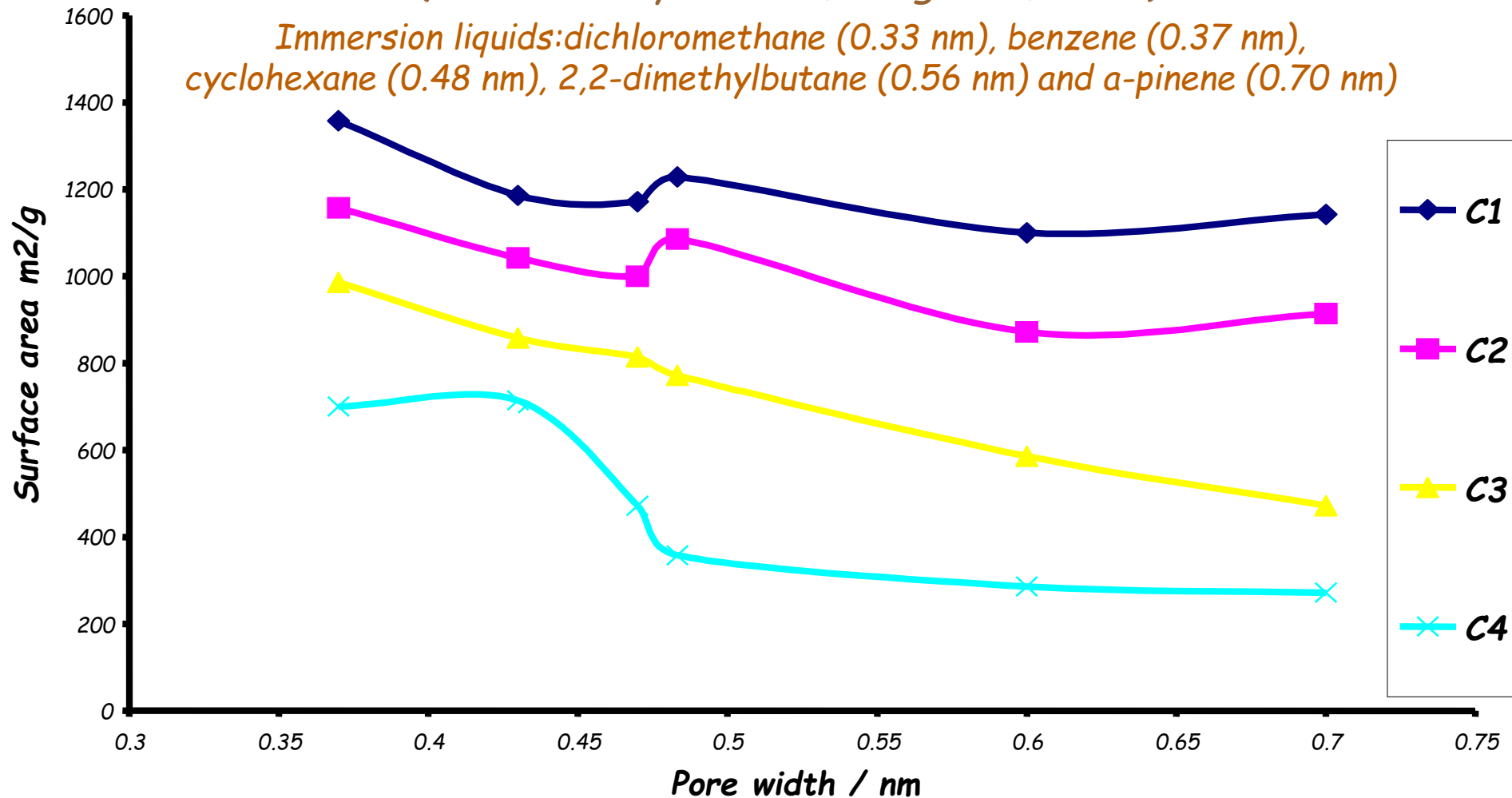
*Possible immersion liquids:*

*Non-polar organics are good candidates. Now, their use is limited those materials they can wet, i.e. essentially carbons*

*Since the accessibility of micropores depends on size of molecules, screening of micropore size can also be done*

*Accessible surface area as a function of probe size  
(= surface area available above a given pore width)  
for carbons with increasing activation from C1 to C4  
(after Denoyel et al., Langmuir, 1993)*

*Immersion liquids: dichloromethane (0.33 nm), benzene (0.37 nm),  
cyclohexane (0.48 nm), 2,2-dimethylbutane (0.56 nm) and  $\alpha$ -pinene (0.70 nm)*



## D/ Three applications of immersion calorimetry

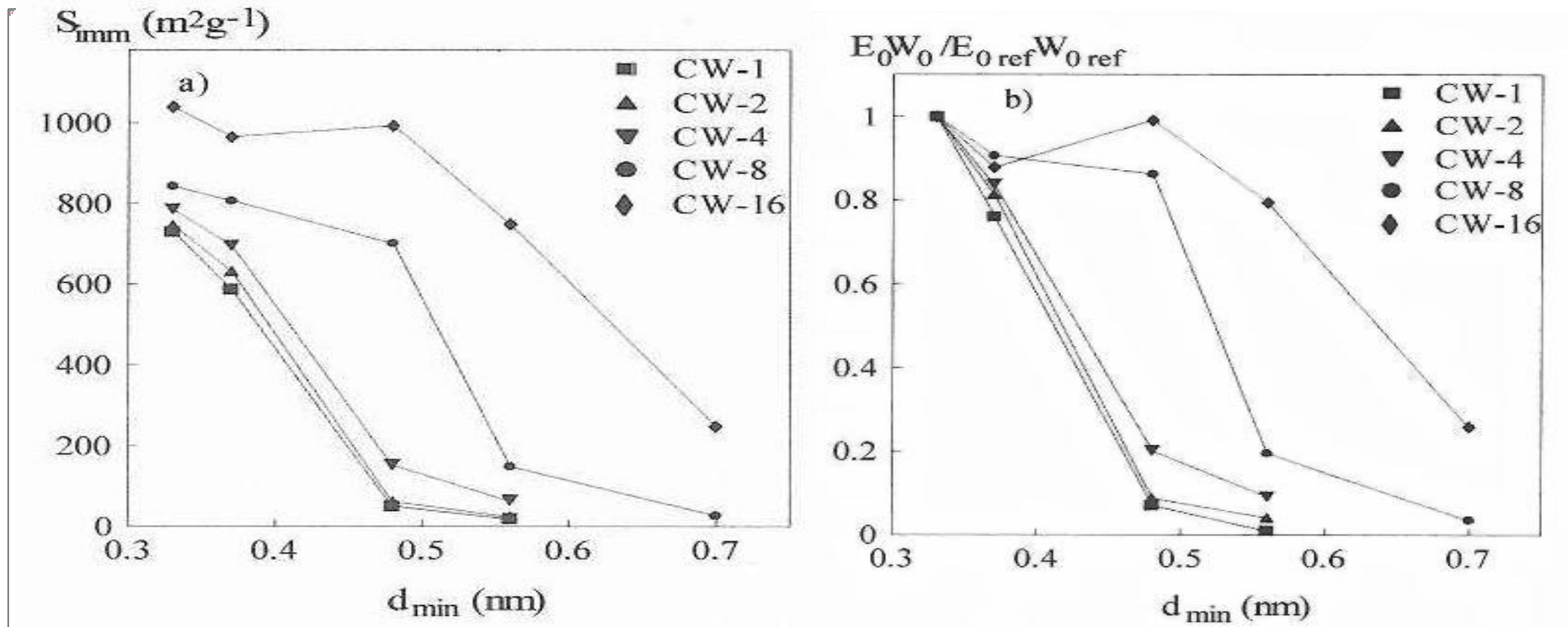
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Immersion calorimetry of a series of activated carbons: *area* accessible to molecules of different size (left) and resulting *pore-size distribution* (right) (after F.Rodriguez Reinoso et al., 2000)

Immersion liquids: dichloromethane (0.33 nm), benzene (0.37 nm), cyclohexane (0.48 nm), 2,2-dimethylbutane (0.56 nm) and  $\alpha$ -pinene (0.70 nm)



# Conclusions

- ⌘ Calorimetry is more than 200 years old, adsorption calorimetry started more than 150 years ago, but there is still much to do
- ⌘ Much work was qualitative (heats). We now must assess energy or enthalpy changes and avoid absolutely the term « heats of adsorption »
- ⌘ This requires much care in designing, analysing and carrying out the experiment
- ⌘ Other calorimetric experiments are available for the study of adsorption or adsorbents:
  - Adsorption calorimetry from solutions
  - Thermoporometry to study the freezing of adsorbate in mesopores and derive the pore-size distribution
  - Desorption calorimetry to apply BJH in the macropore range



*Marsella: ciudad de 2600 años, donde cresce la calorimetria de adsorcion desde 160 años !*

